

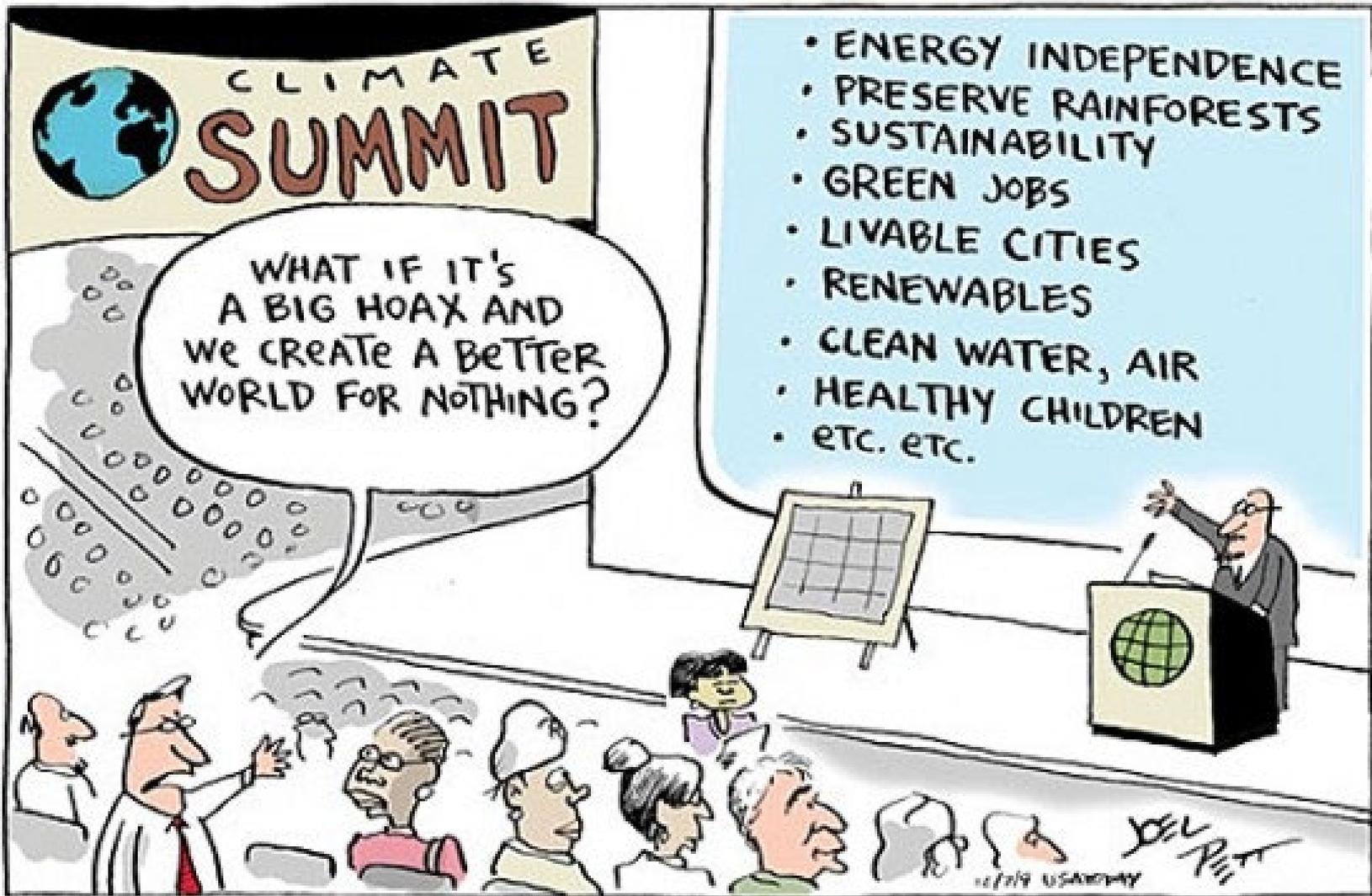
Biomass Utilization & Sustainability of Biofuels

Michael Harasek

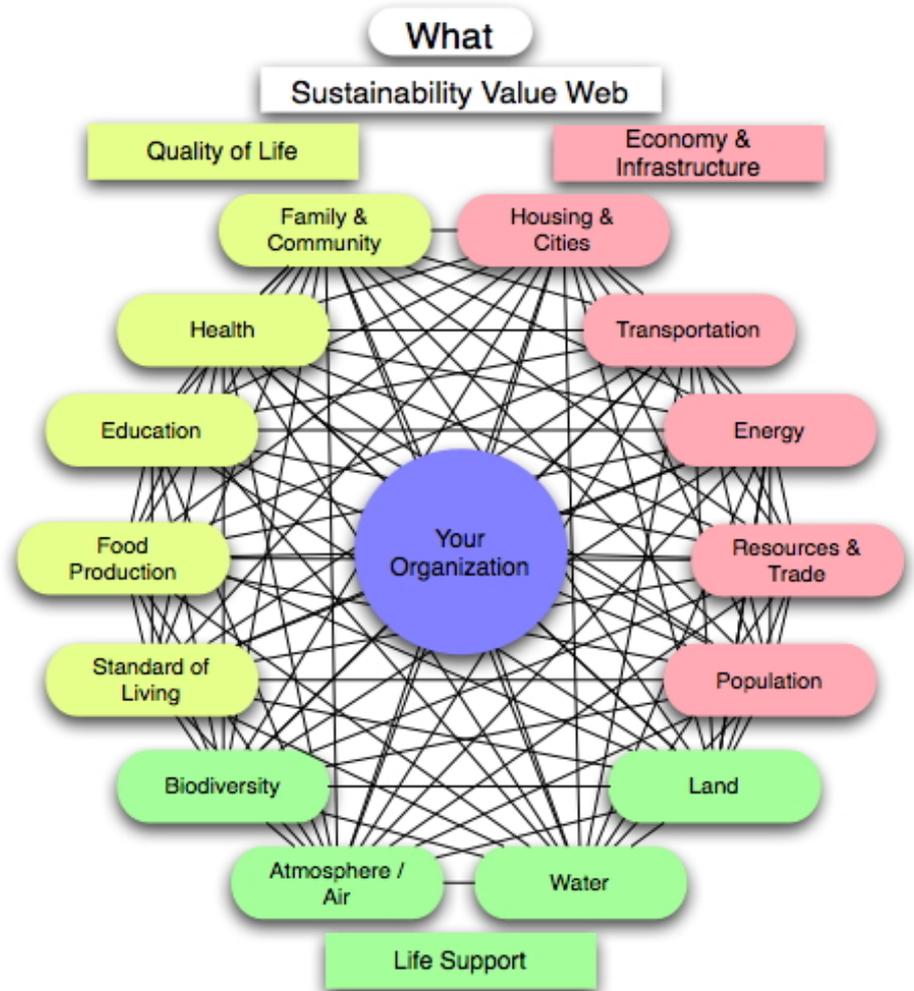
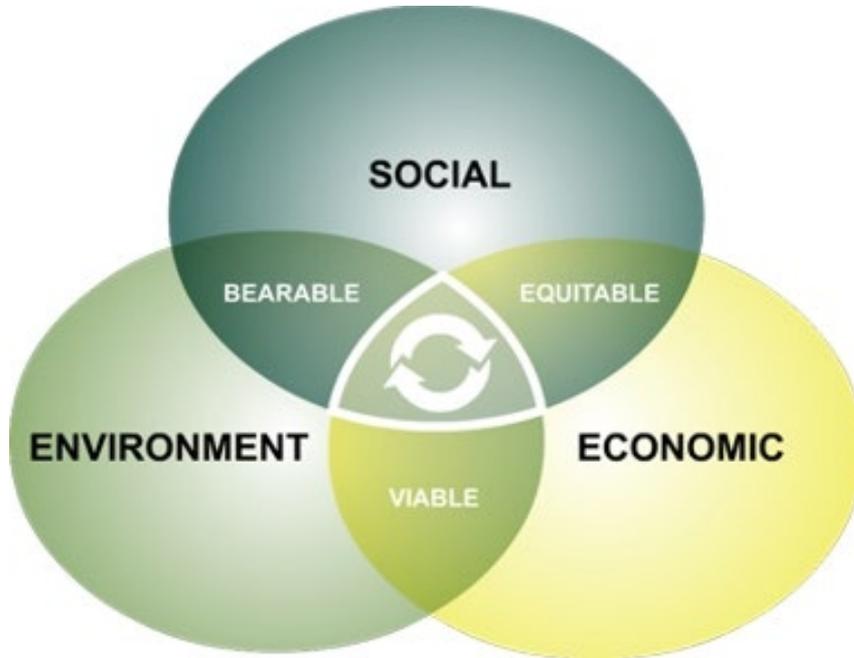
Technische Universität Wien
Institut für Verfahrenstechnik, Umwelttechnik und Technische Biowissenschaften
michael.harasek@tuwien.ac.at

- Introduction
- Sustainability criteria – the European perspective
- Primary energy composition
- Global biomass related issues
- Biomass gasification
- Biogas digestion
- Biomethane for grid injection and as vehicle fuel
- Hydrogen & Power-To-Gas
- Conclusions

Why should we care about sustainability?

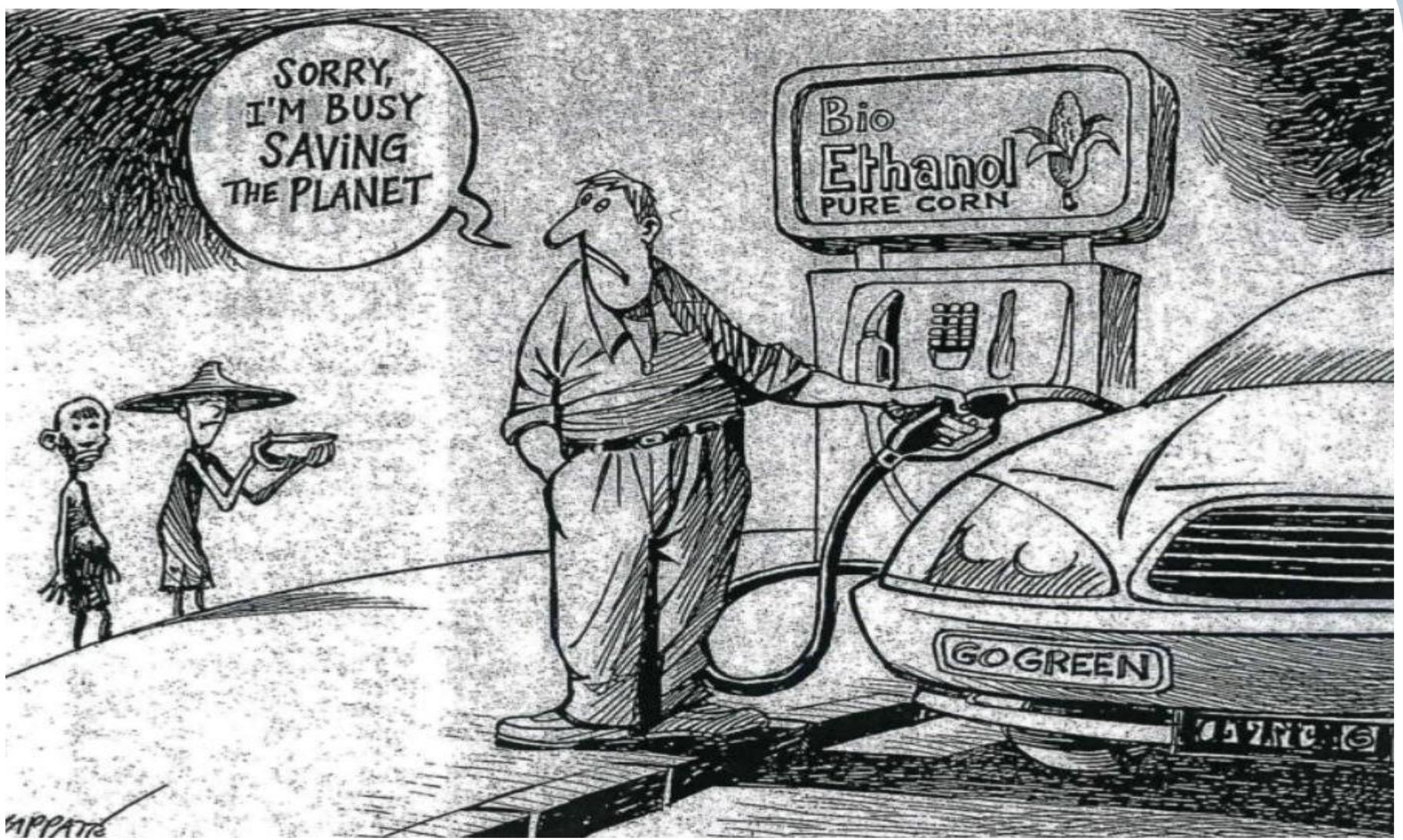


- The **Directive 2009/28/EC** sets out sustainability criteria for biofuels in its articles 17, 18 and 19. These criteria are related to greenhouse gas savings, land with high biodiversity value, land with high carbon stock and agro-environmental practices.
- The **criteria apply since December 2010**. The European Commission (EC) has adopted a number of Decisions and Communications to assist the implementation of the EU's sustainability criteria.



✓ Sustainability involves all aspects of life

Are new Biofuels the Solution?



Source: IHT 11-04-2008

- EU Directive 2009/28/EC (Renewable energy directive: RED) requires:
- Proof of sustainability of biomass:
 - no production from no-go areas (high biodiversity or high carbon stocks),
 - sustainability of production and operations
 - monitor social sustainability and food security
- Raw material should not be obtained from :
 - wetlands
 - continuously forested areas
 - from areas with 10-30% canopy cover
 - from peatlands
 - if the status of the land has changed compared to its status in January 2008
- GHG savings:
 - biofuels and bio-liquids must yield a GHG emission savings of at least 35%
 - (50% from 2017, 60% from production started after 2017)
- Traceability and mass balance must be assured

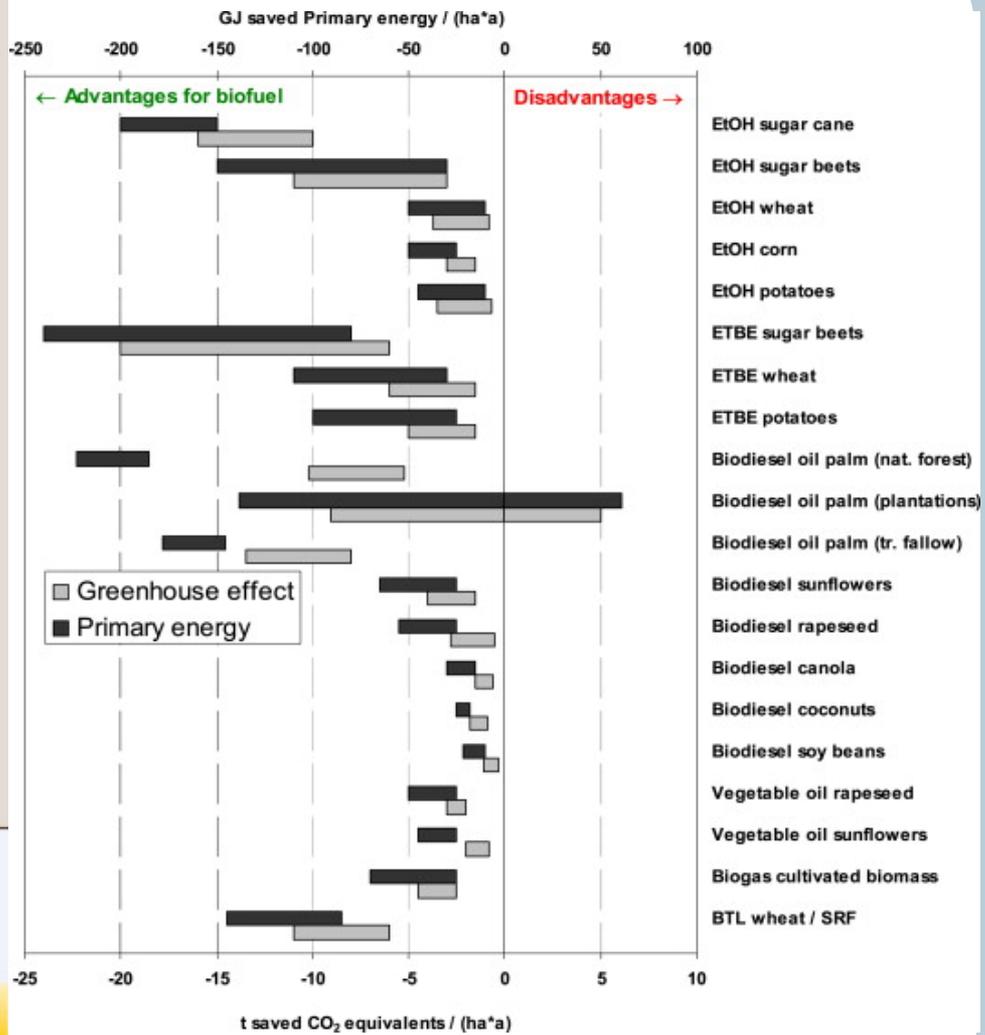
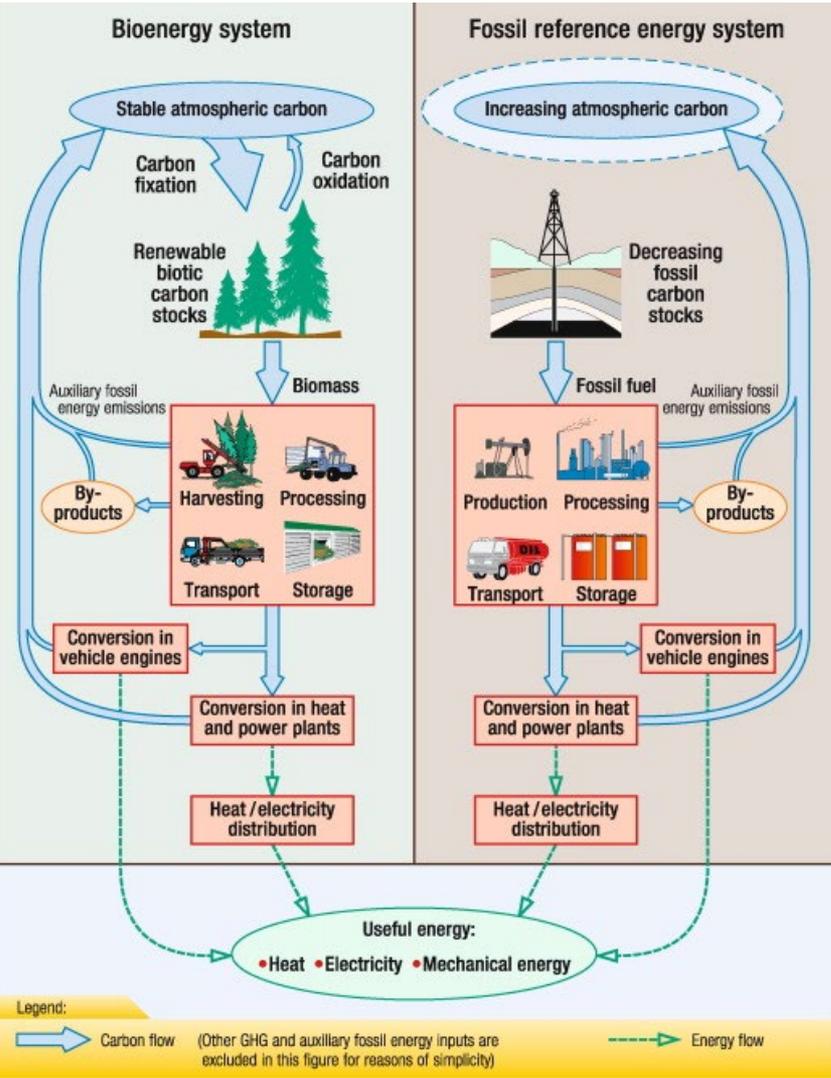


- Includes all process steps (life-cycle) (Annex VII.C)
- End-use efficiency may be taken into account
- Land use change has to be taken into account
- Carbon capture and storage/ replacement

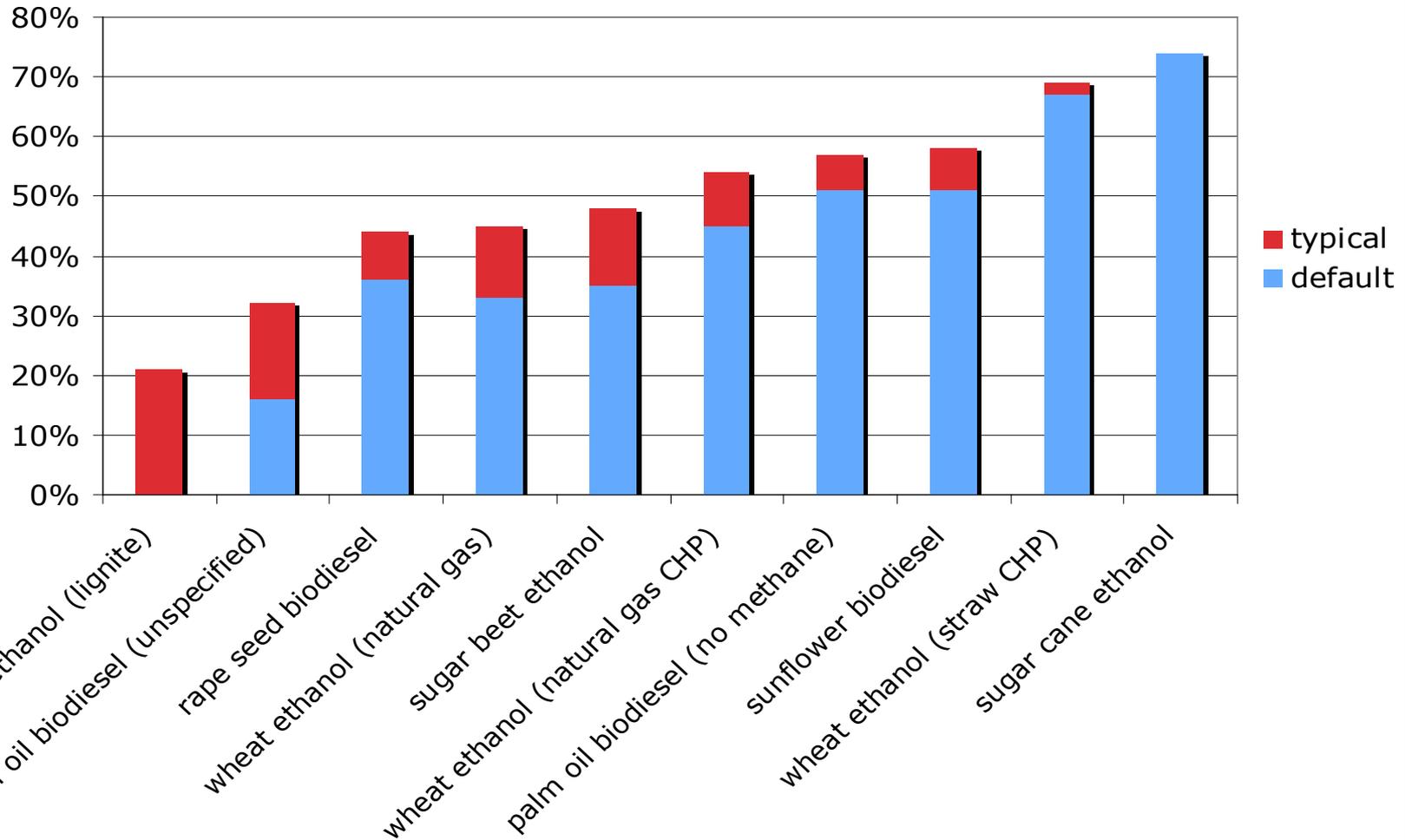
- Co-products by energy allocation, except:
 - agricultural crop residues (not counted)
 - surplus electricity from CHP (special rule)

- Special rule for biofuels from wastes/ residues
- Comparison with EU average for petrol & diesel

Baselines: GHG Emissions of Fuels



Greenhouse gas savings from important first generation biofuels (lifecycle basis)



Trade... or will the fuel be used locally?

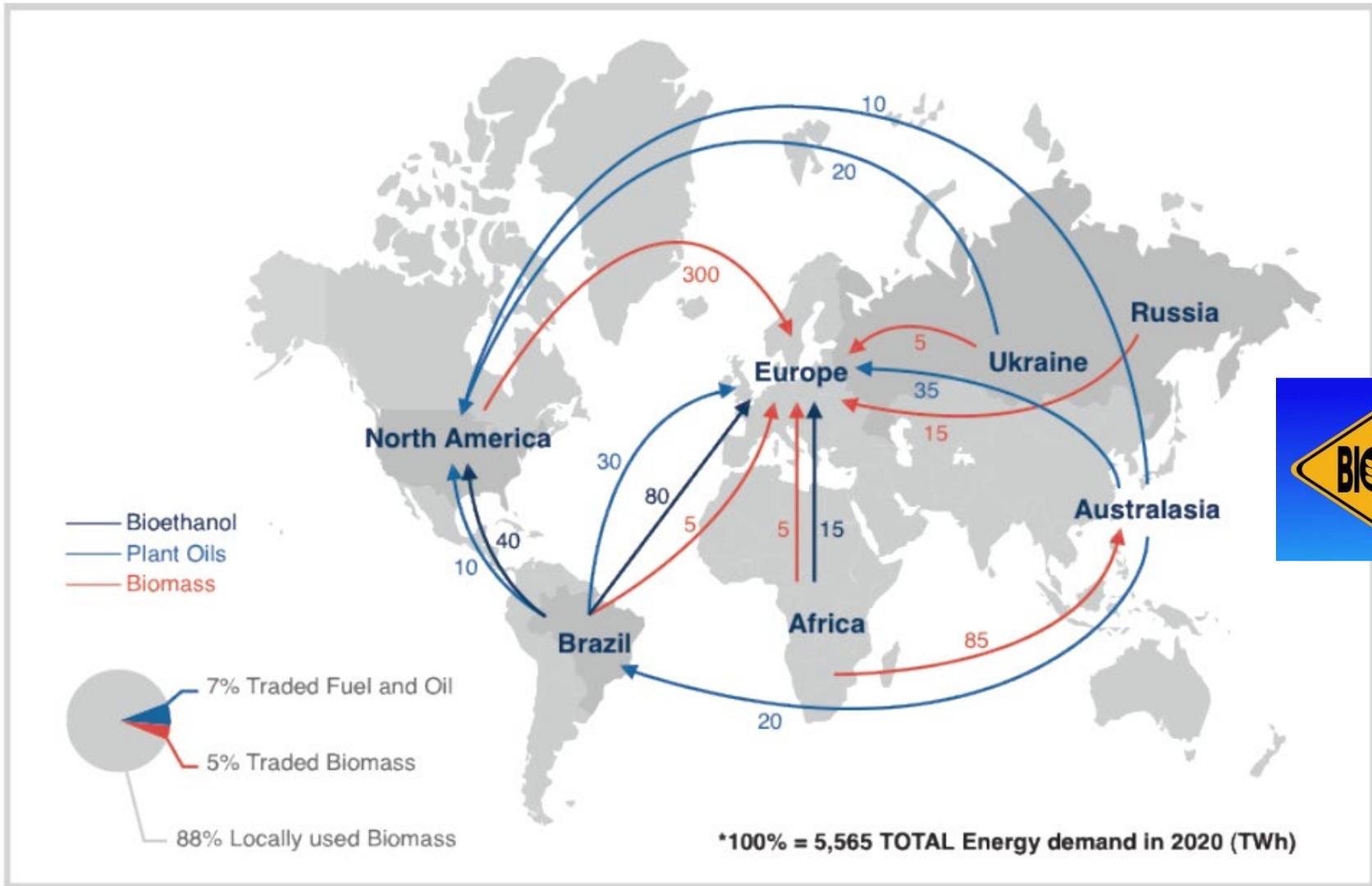
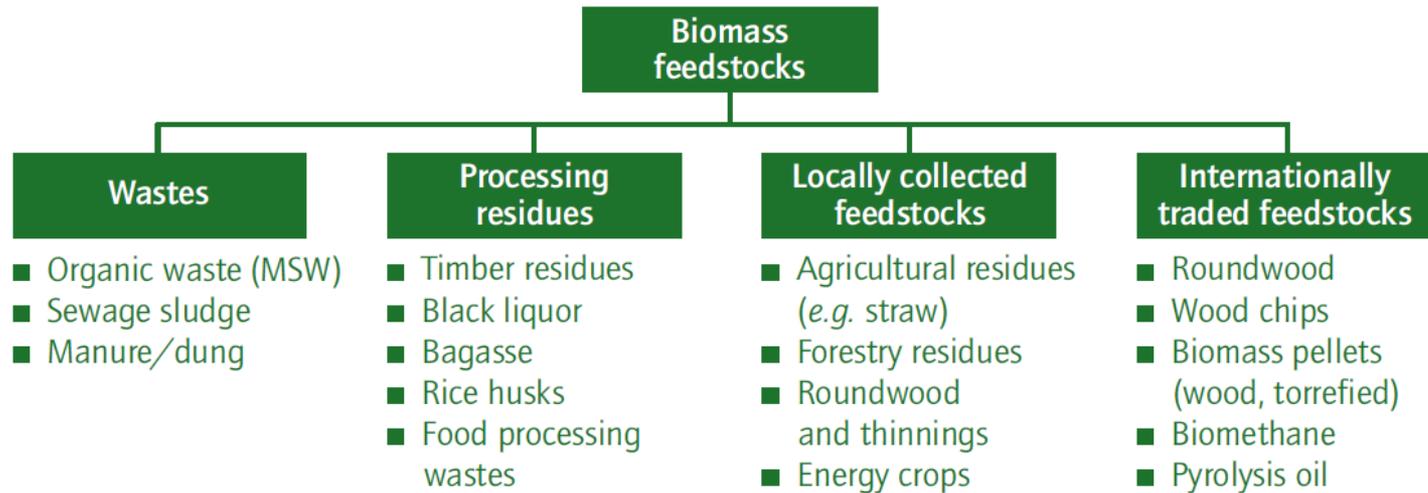


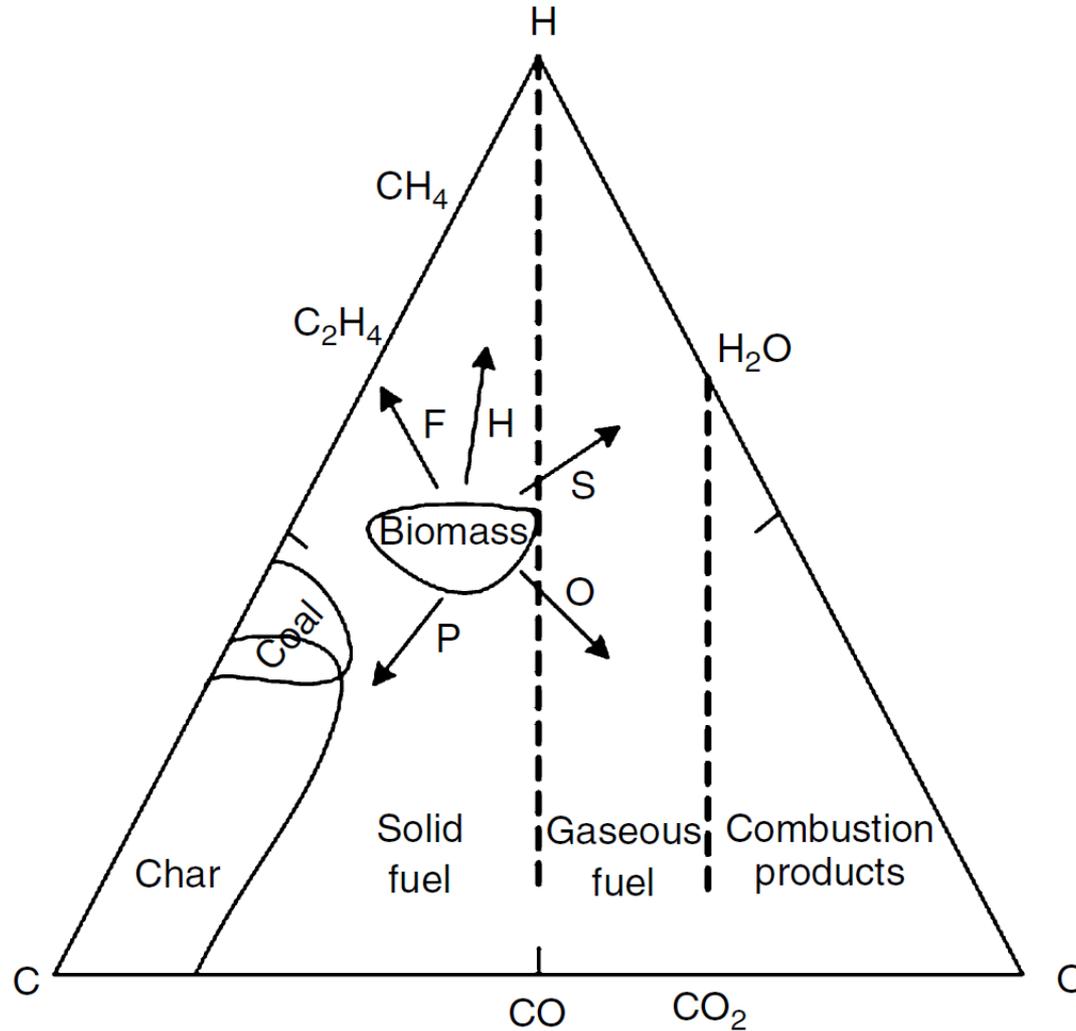
Figure 5: *Expected Biomass Trade Routes*. Values represent final energy demand in 2020.



| | | | | |
|--------------------------------------|---------------|----------|---------|--------|
| Typical feedstock costs (USD/GJ) | negative to 0 | 0 - 4 | 4 - 8 | 8 - 12 |
| Typical plant capacity (MW electric) | 0.5 - 50 | 0.5 - 50 | 10 - 50 | > 50 |

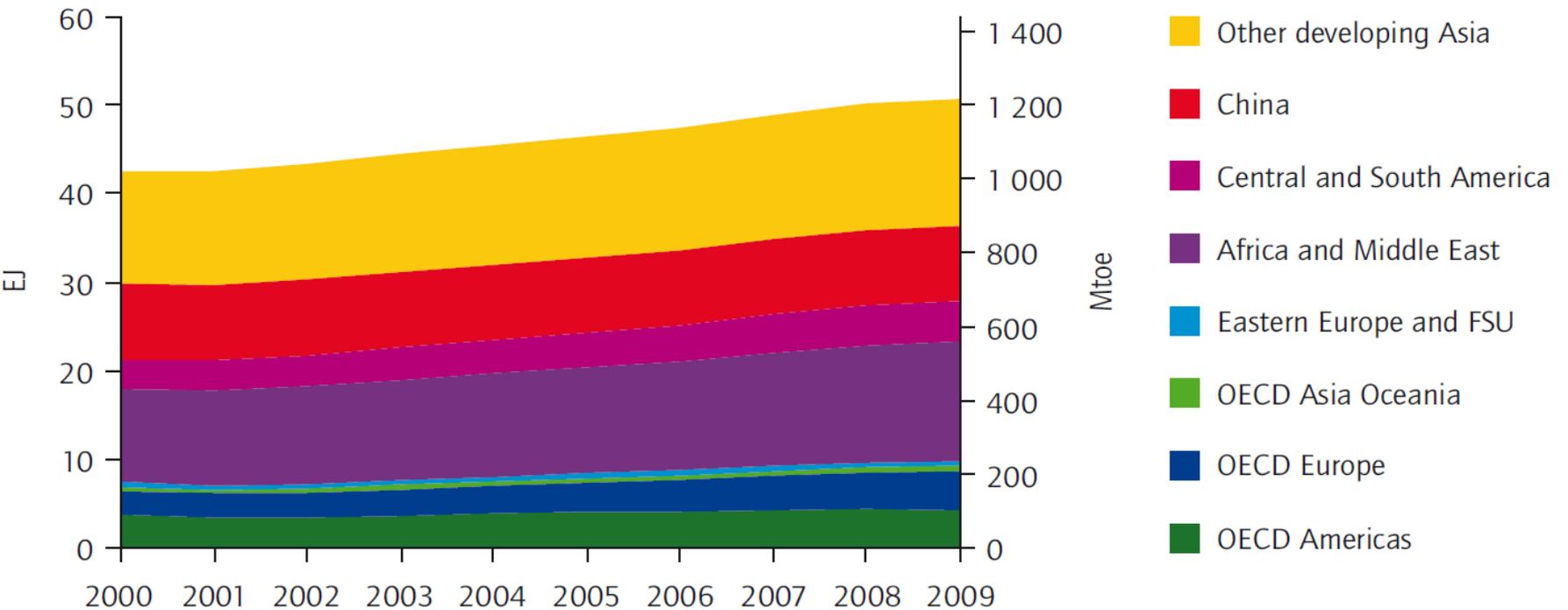
Examples of different biomass feedstocks, typical feedstock costs, and plant capacities

Source: IEA (2012)



H hydrogen S steam O oxygen P slow pyrolysis
 F fast pyrolysis L lignin C cellulose/hemicellulose

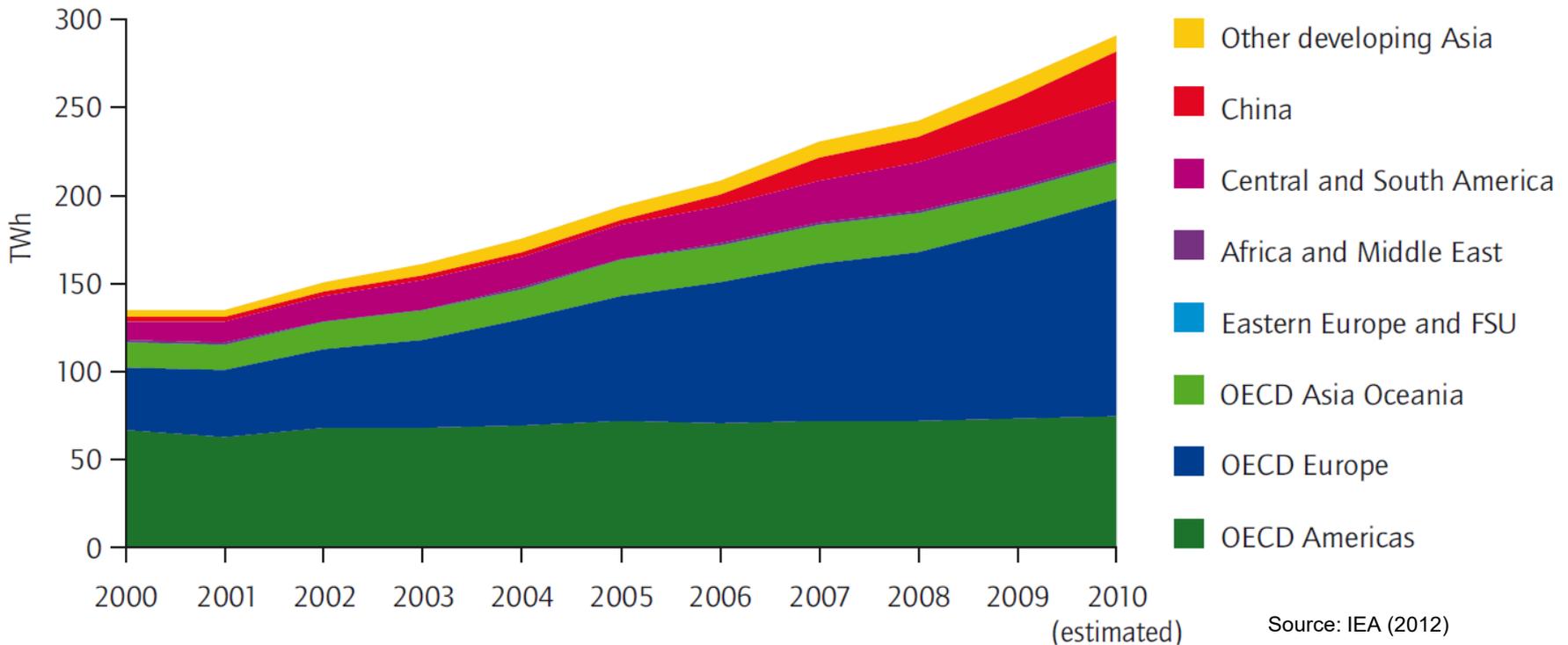
Composition triangle C/H/O (mol/mol)



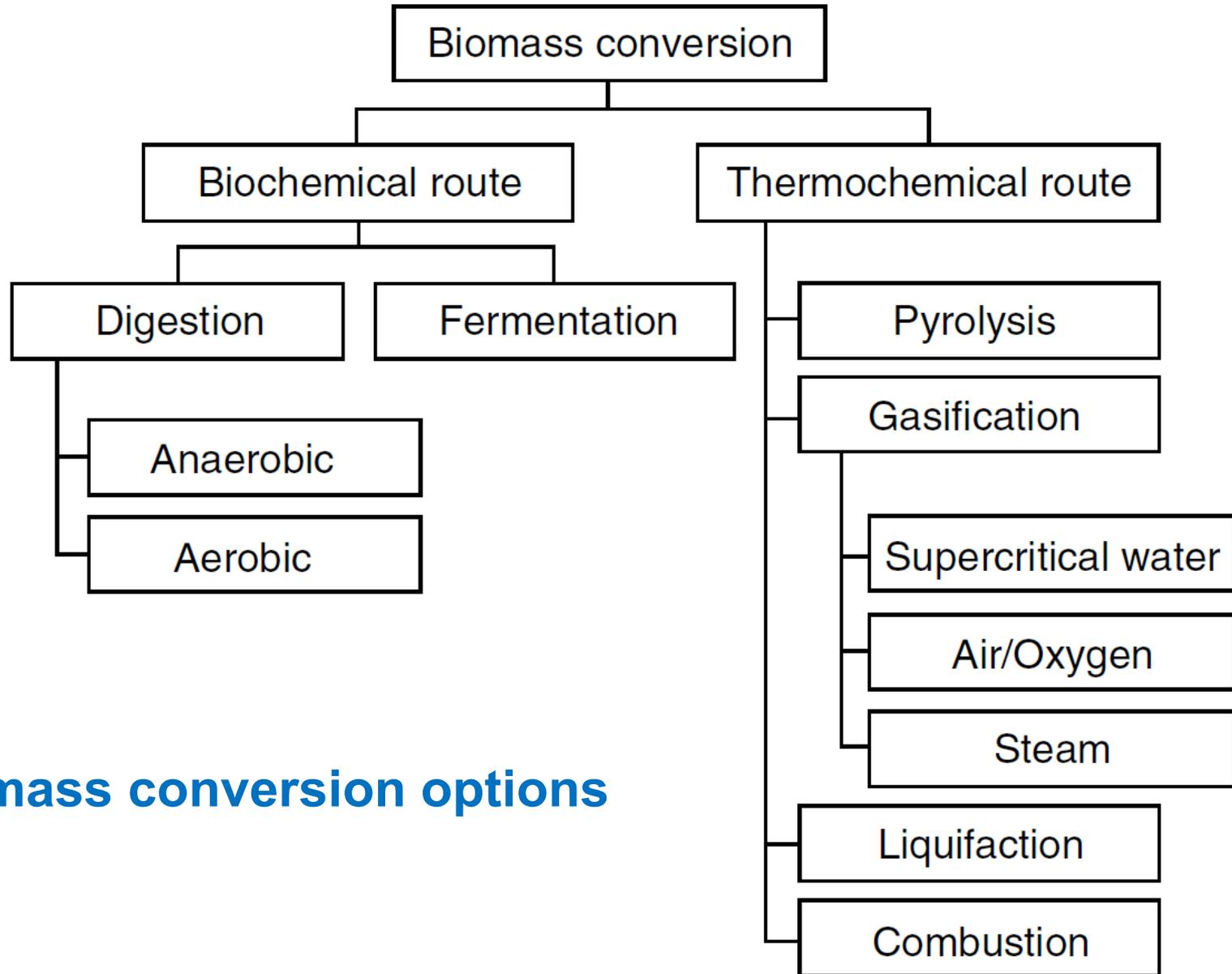
Source: IEA (2012)

Global primary bioenergy supply 2000-2009

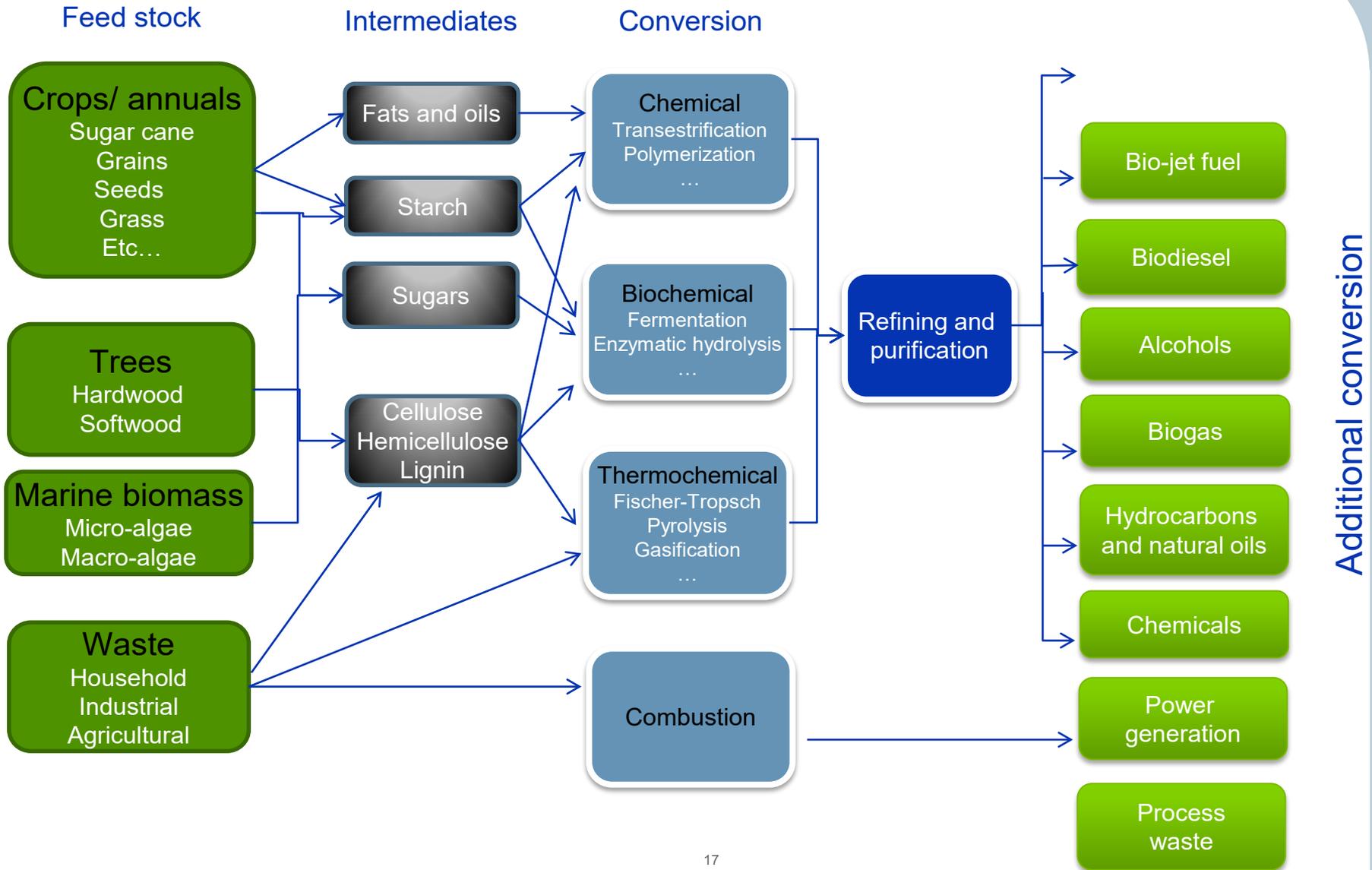
Electricity from Biomass – Global Perspective



Global bioenergy electricity generation 2000-2010



Biomass conversion options



Biomass Utilization Options

| | Basic and applied R&D | Demonstration | Early commercial | Commercial |
|-------------------------------------|------------------------|--------------------|--------------------------|--|
| Biomass pretreatment | Hydrothermal treatment | Torrefaction | Pyrolysis | Pelletisation/ briquetting |
| Anaerobic digestion | Microbial fuel cells | | | 2-stage digestion 1-stage digestion Biogas upgrading Landfill gas Sewage gas |
| Biomass for heating | | | Small scale gasification | Combustion in boilers and stoves |
| Biomass for power generation | | | | |
| Combustion | | Stirling engine | Combustion with ORC | Combustion and steam cycle |
| Co-firing | | Indirect co-firing | Parallel co-firing | Direct co-firing |
| Gasification | Gasification with FC | BICGT BIGCC | Gasification with engine | Gasification with steam cycle |

Note: ORC = Organic Rankine Cycle; FC = fuel cell; BICGT = biomass internal combustion gas turbine; BIGCC = biomass internal gasification combined cycle

Technology status of biomass utilization options

Source: Bauen et al. (2009), IEA (2012)

Bioenergy

- Bioenergy represents over 10% of global primary energy supply
- Primary bioenergy demand > 50 EJ (end of 2011)

Biomass use:

- 86% for cooking, heating & cooling (only 25% modern bioenergy)
- **10,5% for power generation**
- 3,5% for transport fuels

Biomass electricity

- 70 GW of biomass power generation capacity end of 2011, over 65 GW in 2010
- Production in power-only and CHP plants by direct firing or co-firing
- (EU in 2010: 36 % power only , 64 % CHP)
- 88 % derived from solid biomass (US, EU, Brazil, China)



Source: Renewable Energy Policy Network for the 21st Century (2012)

Consequences of policies to reduce GHG and to diversify energy source

- Increasing demand for biomass fuels
- Local feedstock not sufficient to cover demand
- increasing international trade of biomass fuels
- creation of large feedstock plantations in tropical & sub-tropical regions (often corporate investments)

Increasing size of bioenergy power facilities over the last decade:

- 20 MW → 750 MW in the UK (conversion of coal-fired power plant)
- Trend is enhanced because of co-firing developments

Locally used biomass versus internationally traded biomass

New challenges

- Ensure sustainability of modern bioenergy
- Develop and report on local bioenergy

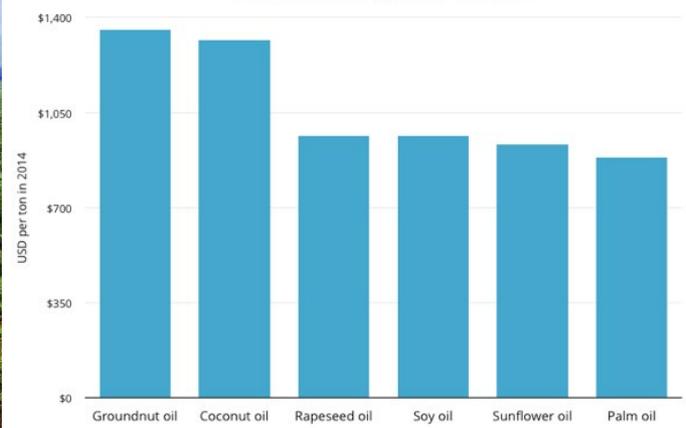


Palm Oil Production & Sustainability

Palm Oil Production



International Vegetable Oil Prices



Source: FAOstat



Source: FAO International Commodity Prices



Scale Influence on some Bioenergy Technologies

| | Scale | Power range | Thermal efficiency | Electric efficiency |
|---|------------|----------------------------|--------------------|---------------------|
| Heating (boiler) | Small | 25 – 100 kW _{th} | 80 – 85 % | |
| | Medium | 100-500 kW _{th} | 85 – 87 % | |
| | Large | 500-5000 kW _{th} | 87 – 93 % | |
| CHP (boiler + steam turbine) | Small | 1-10 MW _e | 63 – 70 % | 13-21 % |
| | Medium | 10-25 MW _e | 59 – 63 % | 21-26 % |
| | Large | 25-50 MW _e | 52 – 59 % | 26-35 % |
| CHP (gas engine) | Small | 0.1- 0.25 MW _e | | 31 – 33 % |
| | Medium | 0.25 -1 MW _e | | 33 – 38 % |
| | Large | 1 -2 MW _e | | 38 – 40 % |
| CHP (diesel engine) | Small | 0.1 – 0.75 MW _e | 46 – 50 % | 37-42 % |
| | Medium | 0.75 -1.5 MW _e | 45 – 50 % | 42-44 % |
| | Large | 1.5 - 5 MW _e | 44 – 45 % | 44-45 % |
| Co-firing Coal power plants (boiler + steam turbine) | Only Large | 500 - 750 MW _e | 50 – 52 % | 35-43 % |

Source: Ecofys, EU-Project TREN/A2/143-2007 (2010)

- Grate furnace and fluidized bed technology
- Steam turbines
- Combined heat and power
- Large scale facilities $> 100 \text{ MW}_{el}$

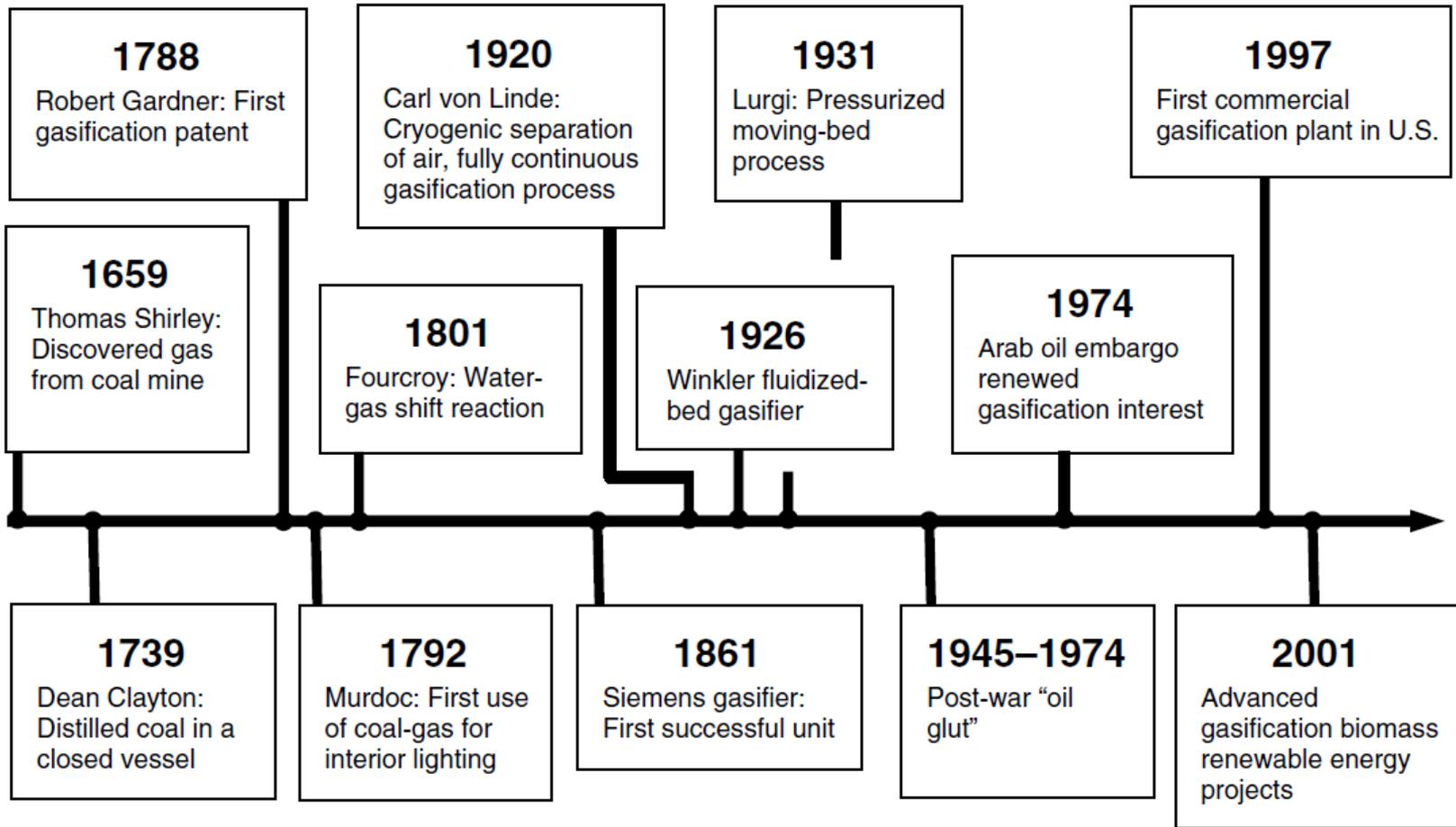




Fray Bentos Pulp Mill produces 200 MW el. (10% of Uruguay's domestic consumption) + 1 Mt/a eucalyptus pulp

Biomass Gasification

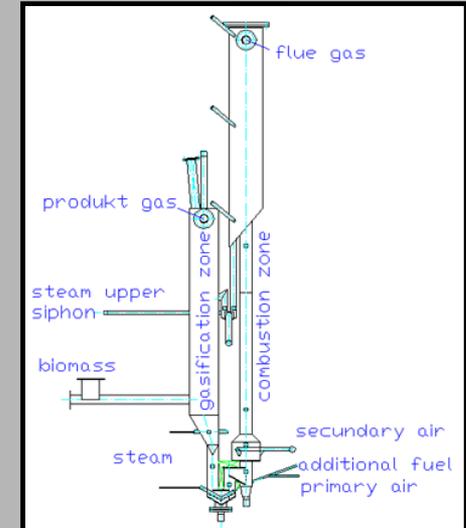
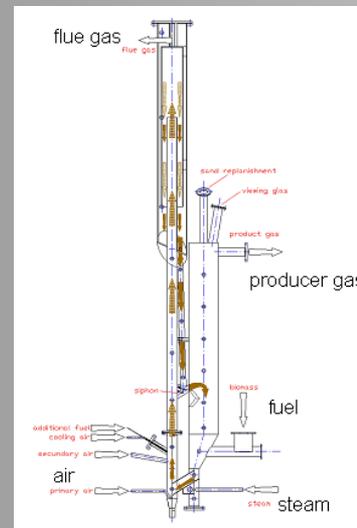
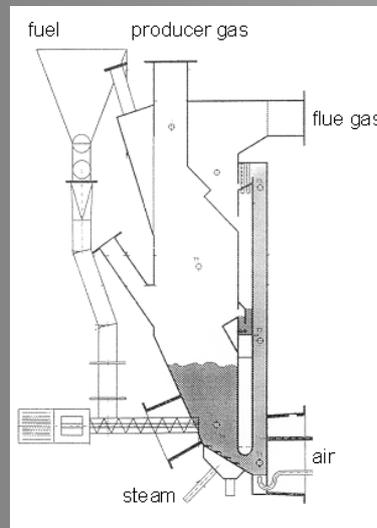
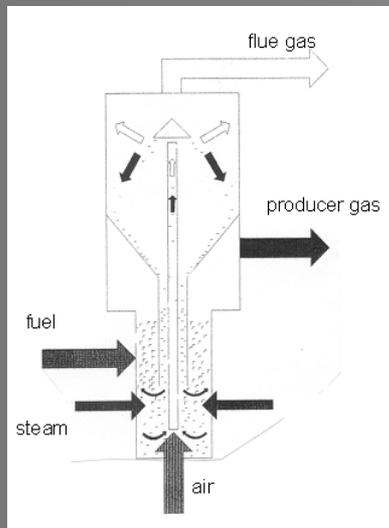
History of Gasification Technology



Source: P.Basu, Academic Press (2010)

Development of fluidized bed steam biomass gasification

Research @ TU Wien – Institute of Chemical Engineering

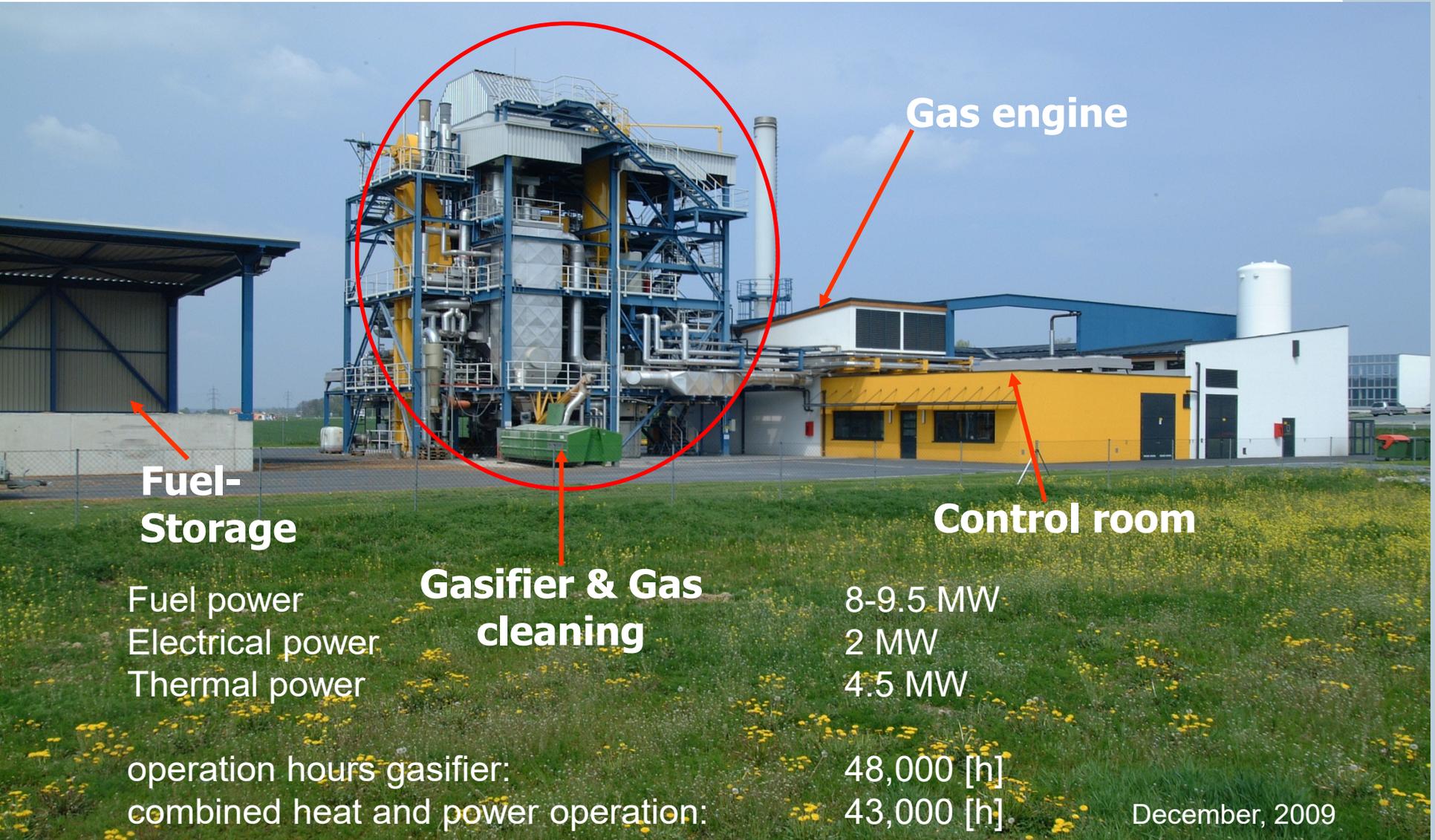


1993 - 1996
FICFB gasifier

1995 - 1999

1999 - 2003

2004 - now
DFB gasifier



Fuel-Storage

Fuel power
Electrical power
Thermal power

Gasifier & Gas cleaning

operation hours gasifier:
combined heat and power operation:

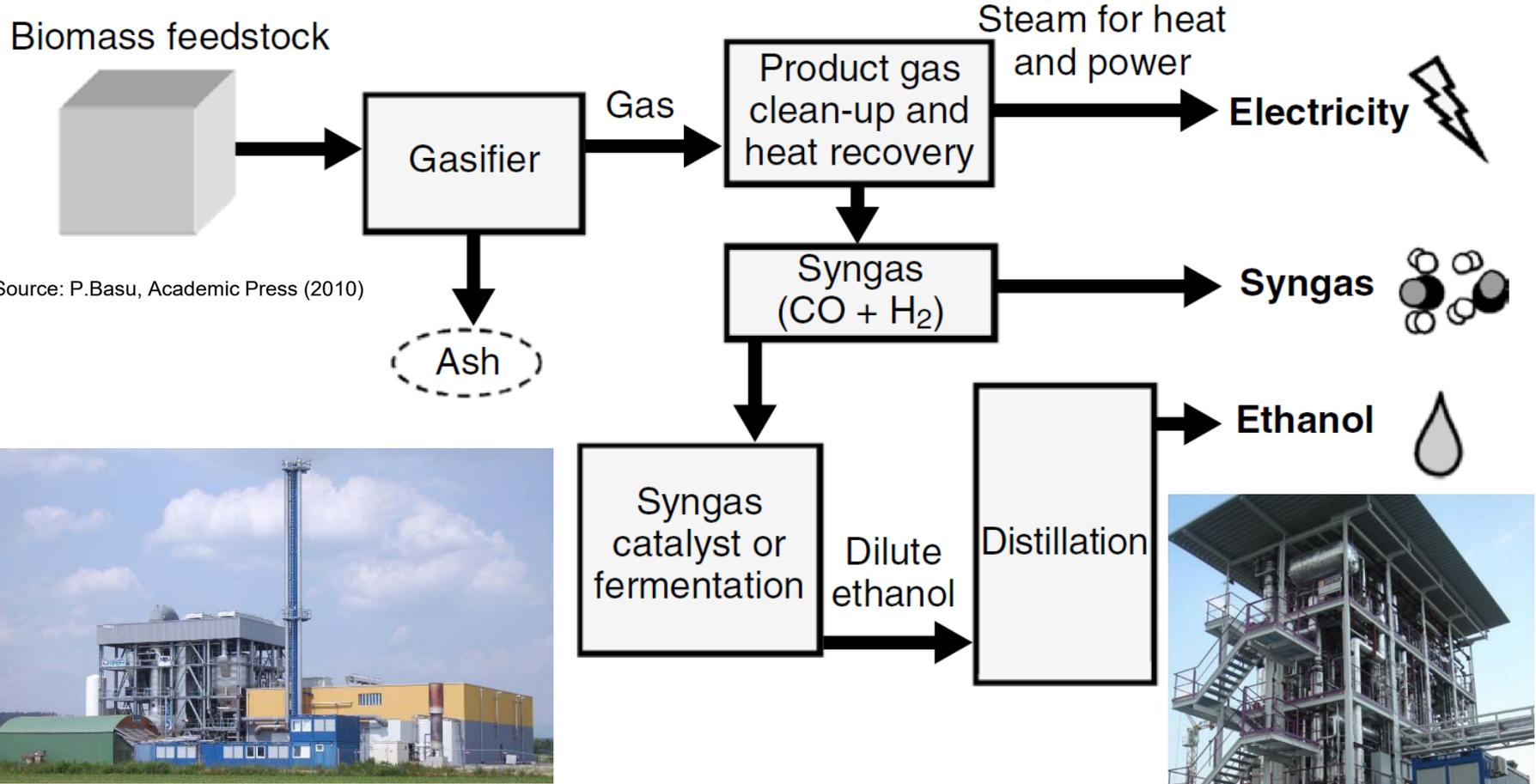
Gas engine

8-9.5 MW
2 MW
4.5 MW

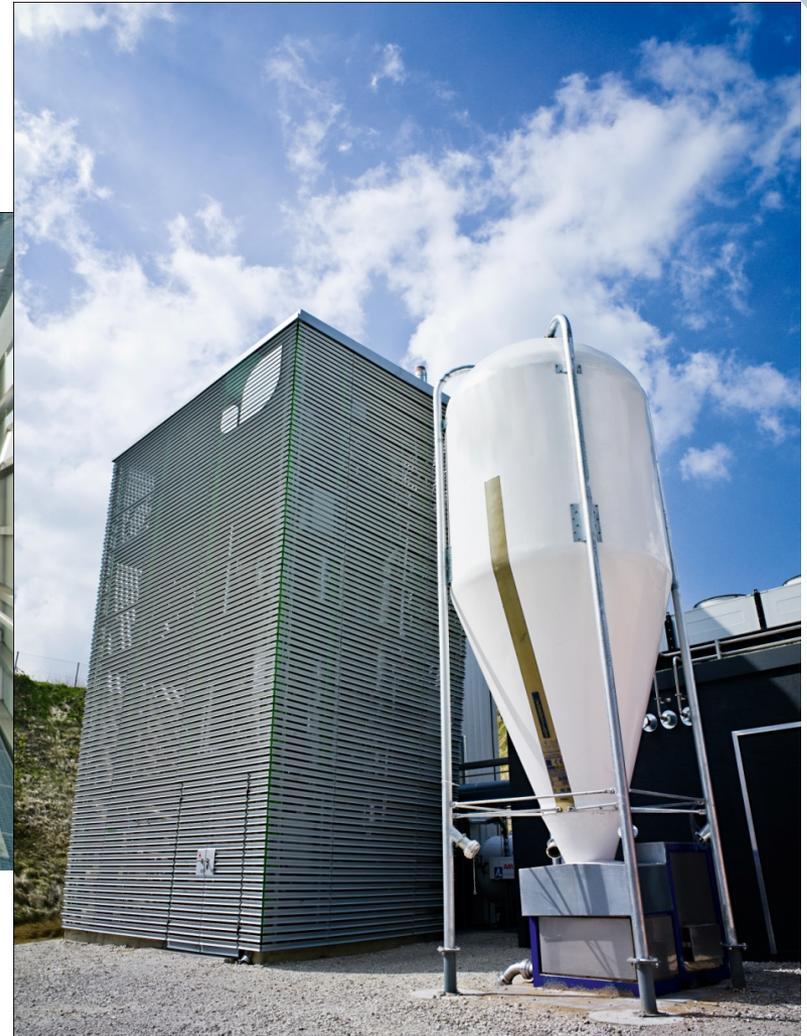
Control room

48,000 [h]
43,000 [h]

December, 2009



Additional options via gasification



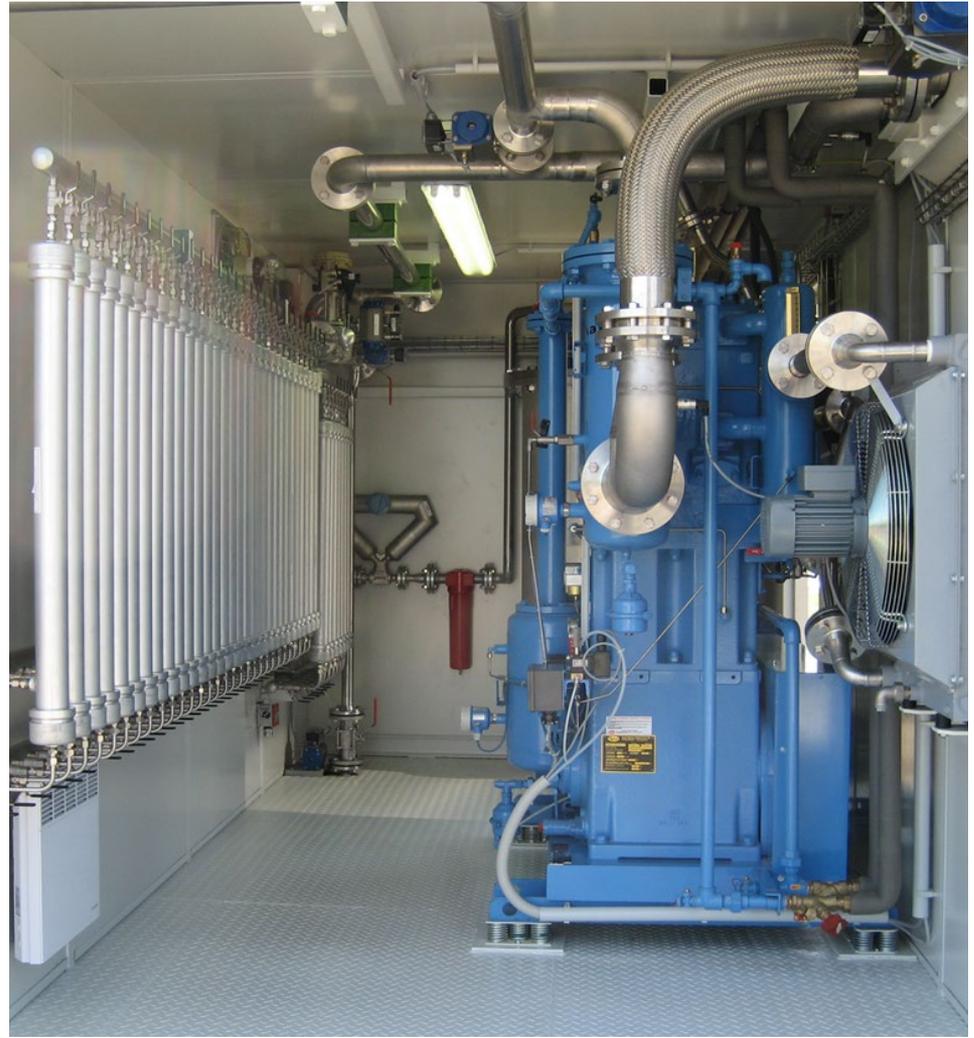
Agnion Heatpipe Reformer Technology for small scale application (e.g. 0,5 - 1 MW_{el})

Biogas Digestion and Grid Injection and Bio-CNG Use



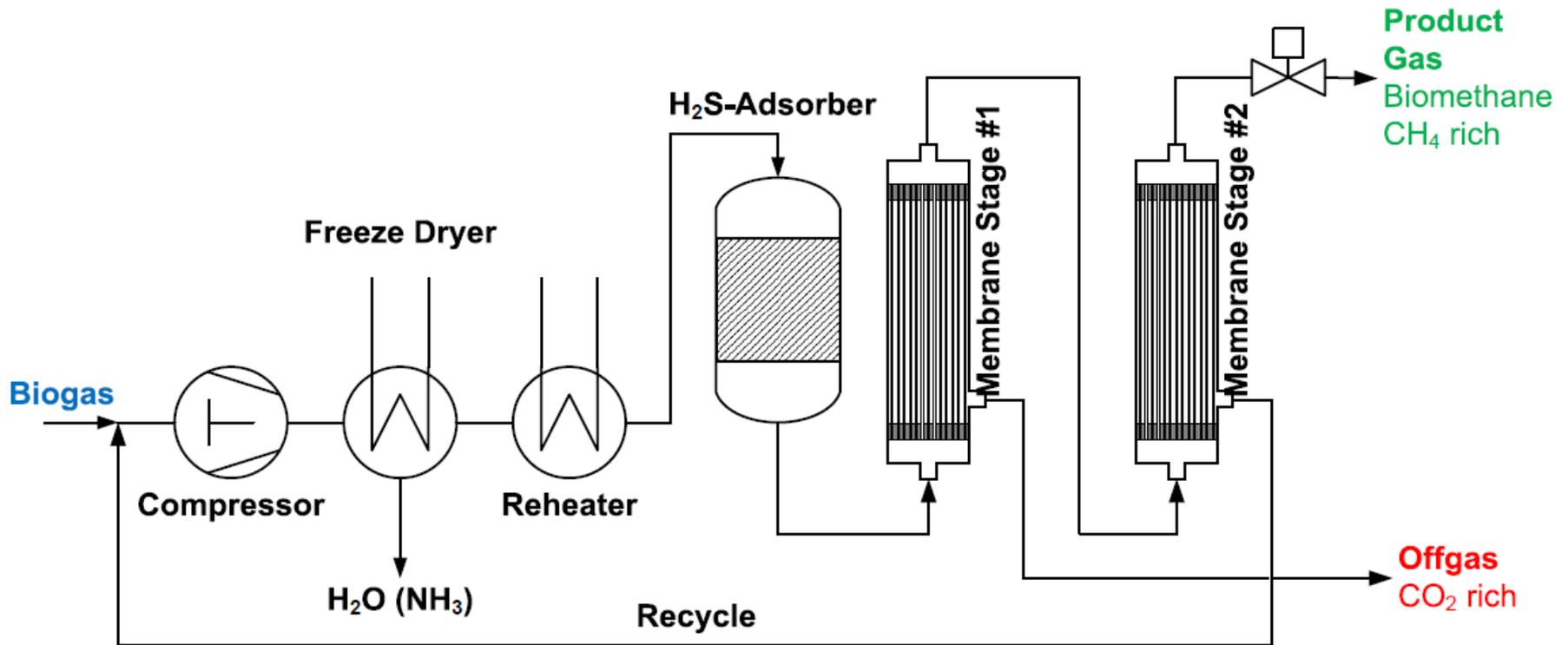
The European Natural Gas Grid

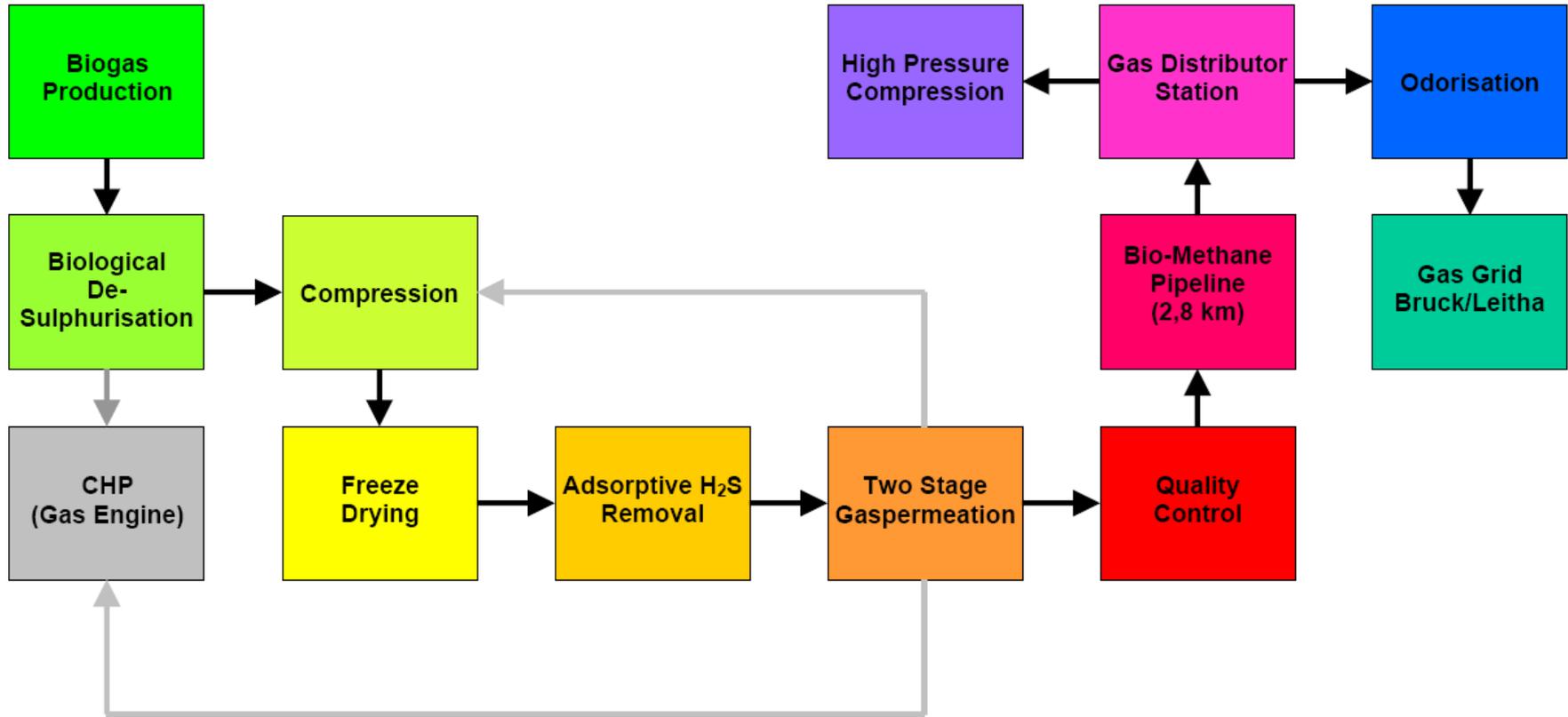
Source: Eurogas (2005)



- Axiom – Membrane separation (180 m³/h biogas)

Process Scheme of a Two-stage Membrane System





- **Biological desulphurisation prior to membrane treatment**
- **Permeate is recycled to CHP plant – „zero methane“ emission of upgrading system**



Permeate recycle to CHP plant

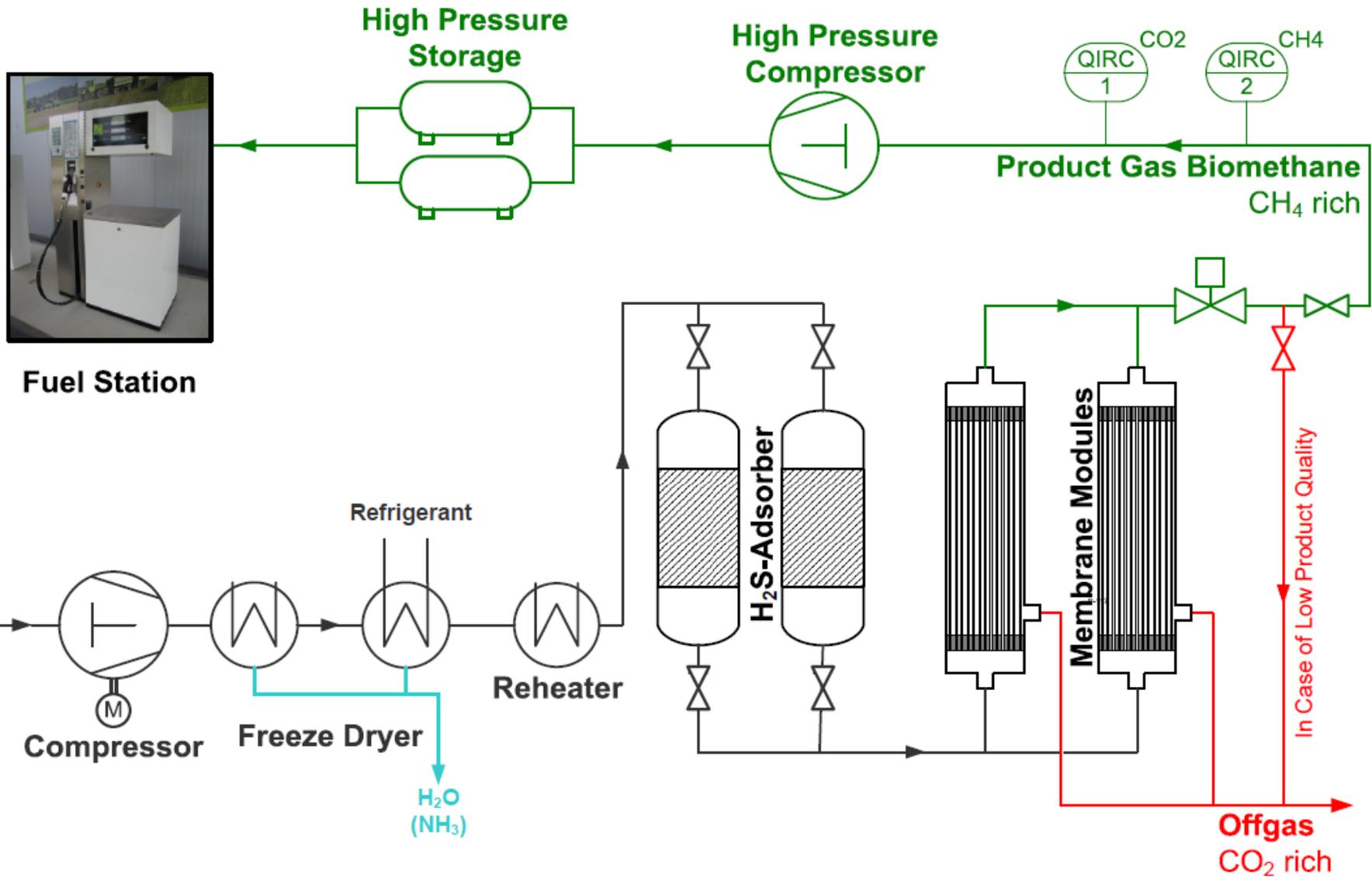
Further information: www.methapur.com

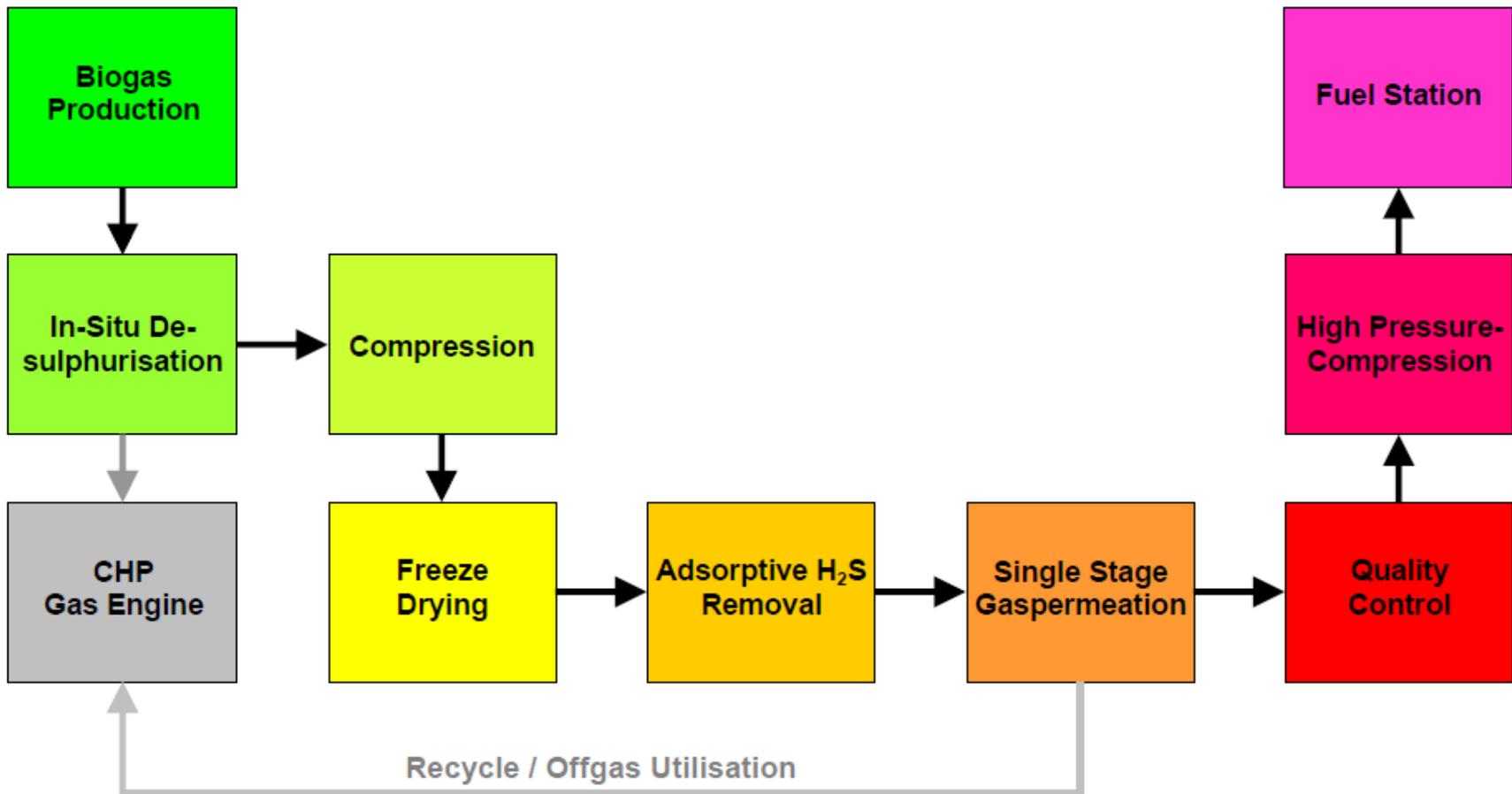
Biomethane fuel station Margarethen/Moos



- Capacity: 500 kg/d bio-methane
- Bio-methane as fuel alternative (tractors, harvesting)

Biomethane Fuel Station: Single Stage Upgrading





- In-situ desulphurisation (addition of iron salts into the fermentation broth to catch sulphides)
- Permeate is recycled to CHP plant – „zero methane“ emission of upgrading system



- Capacity 1,000.000 m³ Bio-methane / a
- BCM (MT-Energie) amine scrubber



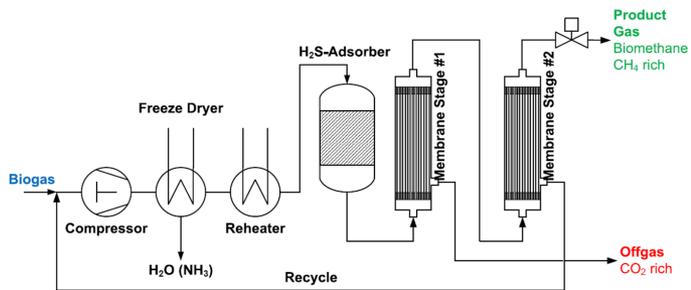
- Capacity: 220 (300) m³/h biogas
- Axiom – Membrane separation

Recent Start-up of First AXIOM Plant in Germany

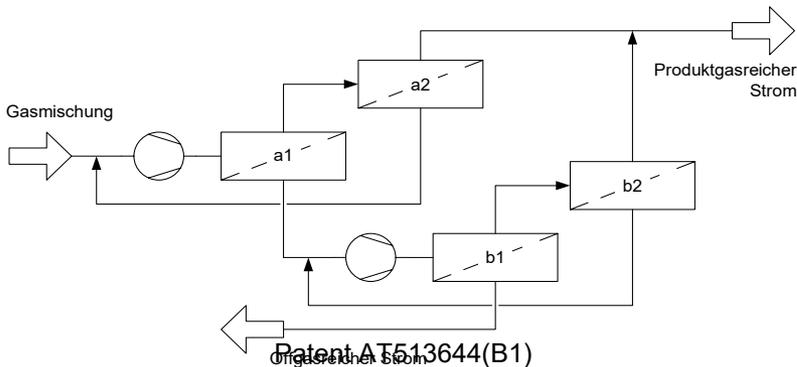


- Capacity 500 m³/h biogas, 300 m³/h biomethane, approx. 8 km pipeline for grid injection and high pressure compression to 60 bar

✓ Process design from 2006:



✓ New process design:



Patent AT 513644 (B1)

(19) (11) EP 2 735 355 A1

(12) EUROPÄISCHE PATENTANMELDUNG

(43) Veröffentlichungstag: 28.05.2014 Patentblatt 2014/22 (51) Int. Cl.: B01D 53/22 (2006.01)

(21) Anmeldenummer: 13194642.8 (22) Anmeldetag: 27.11.2013

(84) Benannte Vertragsstaaten: AL AT BE BG CH CY CZ DE DK EE ES FI FR GB GR HR HU IE IS IT LI LT LU LV MC MK MT NL NO PL PT RO RS SE SI SK SM TR Benannte Erreichungsstaaten: BA ME (72) Erfinder: • HARASEK, Michael 1060 Wien (AT) • MAKARUK, Aleksander 1150 Wien (AT) (74) Vertreter: Elmeyer, Wolfgang Haupt & Elmeyer KG Mariettafer Strasse 50 1070 Wien (AT) (71) Anmelder: • Technische Universität Wien 1040 Wien (AT)

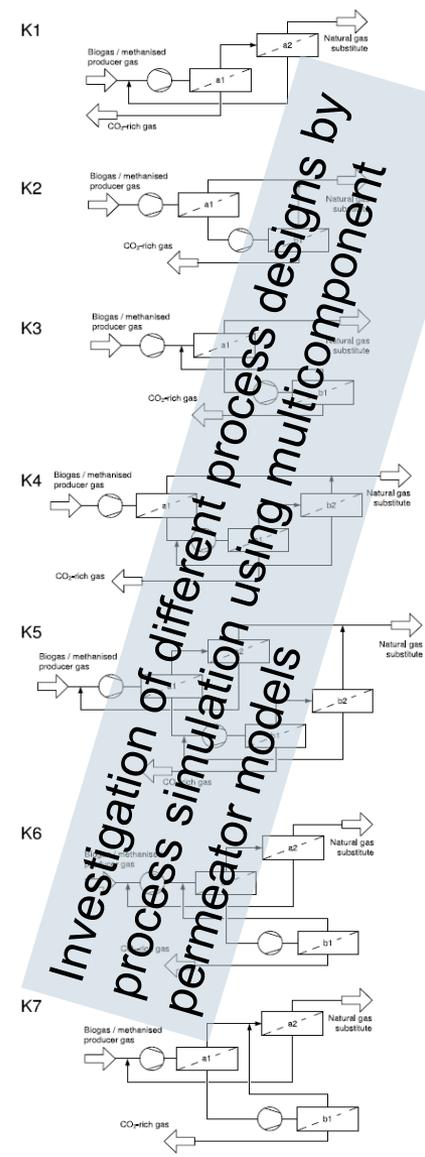
(54) Permeatorsystem zur Trennung von Gasgemischen

(57) Die Erfindung betrifft eine Vorrichtung zur Trennung von im Wesentlichen drucklosen Gasgemischen unter Verwendung von Membran-Gaspermeation, umfassend zumindest zwei Trennstufen, die parallel oder in Serie geschaltet sein können, einen Kompressor zur Bedienung des in einer Freiedlung zugeleiteten Gasgemische mit Druck, gegebenenfalls einen zweiten Kompressor zur Bedienung eines Permeats aus einer Trennstufe mit Druck, sowie zumindest eine Rückführungsleitung für zumindest ein Retenat und/oder Permeat einer Trennstufe, gekennzeichnet durch

- zwei Paare von Trennstufen (a1, a2; b1, b2), die über eine Leitung (R_{a1} , R_{a2}) zur Weiterleitung des Retenats aus der jeweils ersten Trennstufe (a1; b1) eines Paares in die zweite (a2; b2) in Serie geschaltet sind;
- zwei Kompressoren (c1, c2) zur Beaufschlagung des Feeds der jeweils ersten Trennstufe (a1; b1) eines Paares mit Druck;
- eine Leitung (P_{a1}) zur Weiterleitung des Permeats der ersten Trennstufe (a1) eines ersten Paares (a1, a2) zu dem das zweite Trennstufenpaar (b1, b2) mit Druck beaufschlagenden Kompressor (c2);
- je eine Leitung (R_{c1} , R_{c2}) zum Abziehen des Retenats der jeweils zweiten Trennstufe (a2; b2) der Paare;
- je eine Leitung (P_{c1} , P_{c2}) zur Rückführung des Permeats der jeweils zweiten Trennstufe (a2; b2) der Paare; und
- eine Leitung (P_{b1}) zum Abziehen des Permeats der ersten Trennstufe (b1) des zweiten Trennstufenpaares (b1, b2).

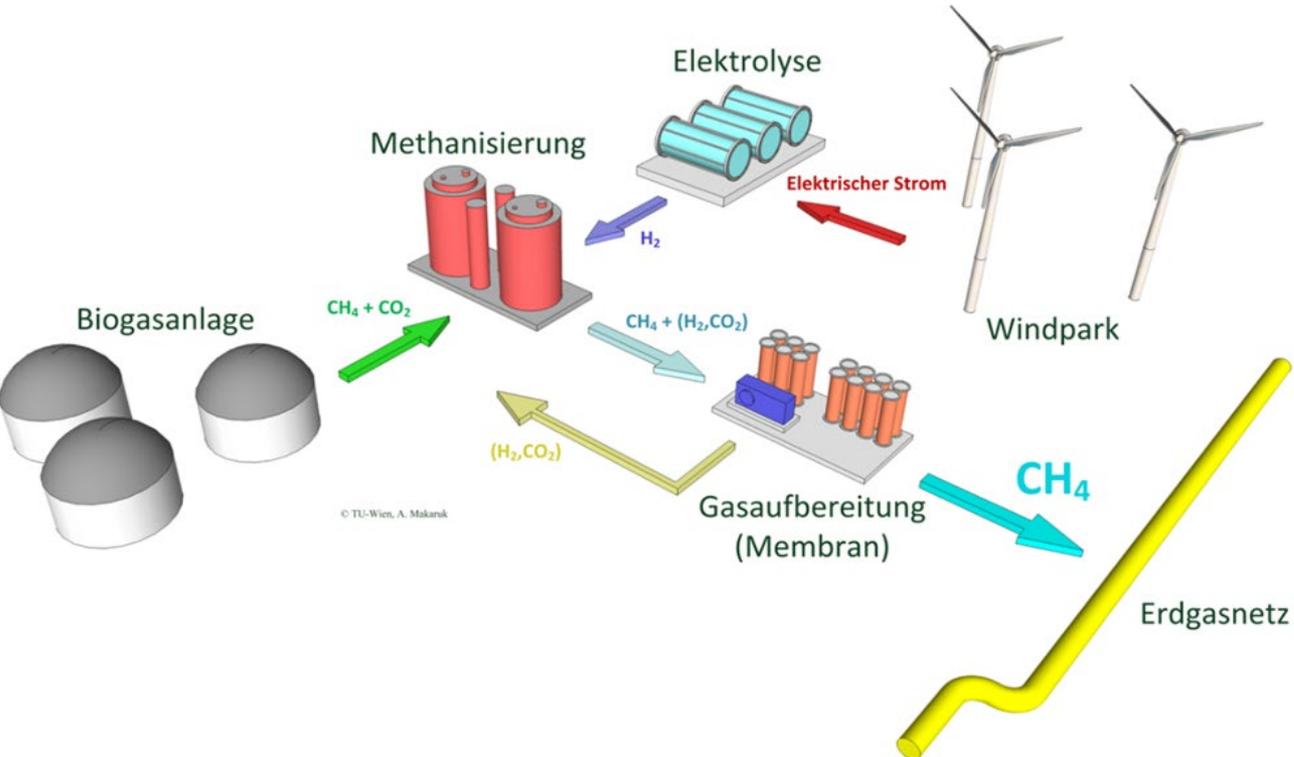
Figur 5

EP 2 735 355 A1



Investigation of different process designs by process simulation using multicomponent permeator models

P2G Integration with Biogas



(19) (10) **AT 514614 B1 2015-05-15**

(12) **Patentschrift**

(21) Anmelde­nummer: A 629/2013 (51) Int. Cl.: C10L 300 (2006.01)
 (22) Anmelde­tag: 05.08.2013
 (45) Ver­öf­fent­lich­am: 15.05.2015

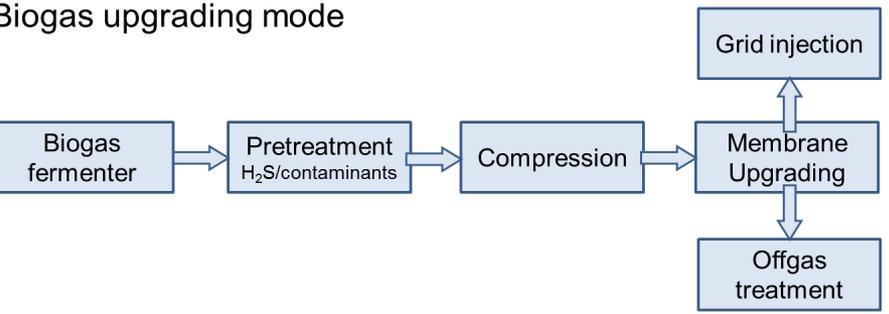
(56) Er­findungs­haltungen: DE 10201116943 A1 (73) Patentinhaber: Technische Universität Wien 1040 Wien (AT)
 DE 102004030717 A1 (74) Ver­tre­ter: HÄUPL & ELLMEYER KG, PATENTANWÄLTEKANZLEI WIEN

(54) **Verfahren und System zum Speichern von Energie**

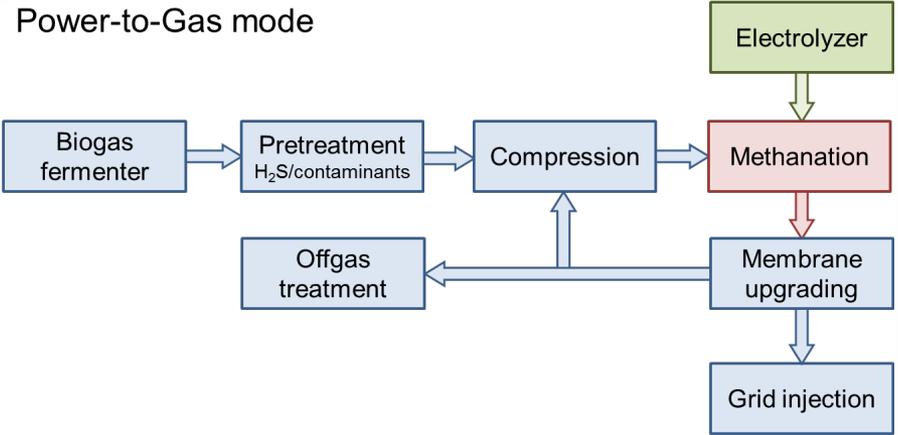
(57) Die Erfindung betrifft ein Energiespeicherverfahren, in dem mit elektrischem Strom durch Wasserelektrolyse H₂ erzeugt wird, weiteres CO₂ erzeugt wird und aus dem H₂ und CO₂ durch Methanisierung CH₄ erzeugt wird und das dadurch gekennzeichnet ist, dass:
 a) das CO₂ neben CH₄ in einer Biogasanlage erzeugt wird;
 b) das CO₂ und CH₄ in einem Membransystem mittels selektiver Gastremmembranen in einen CH₄-reichen Gasstrom und einen CO₂-reichen Gasstrom aufgetrennt werden, wobei der CO₂-reiche Gasstrom durch Methanisierung mit dem erzeugten H₂ zu einem CH₄, CO₂ und H₂ umfassenden Produktgas umgewandelt wird;
 c) zumindest ein Teil des Produktgases in einem Membransystem aufgetrennt wird, um CO₂ und H₂ selektiv von CH₄ abzutrennen; und
 d) dass die Aufreinigung des Biogases und die Aufreinigung des Produktgases der Methanisierung gleichzeitig oder abwechselnd in demselben Membransystem unter Verwendung von Gastremmembranen durchgeführt werden, die zu einer selektiven Abtrennung von CO₂ und H₂ von CH₄ in der Lage sind.

AT 514614 B1 2015-05-15

Biogas upgrading mode



Power-to-Gas mode



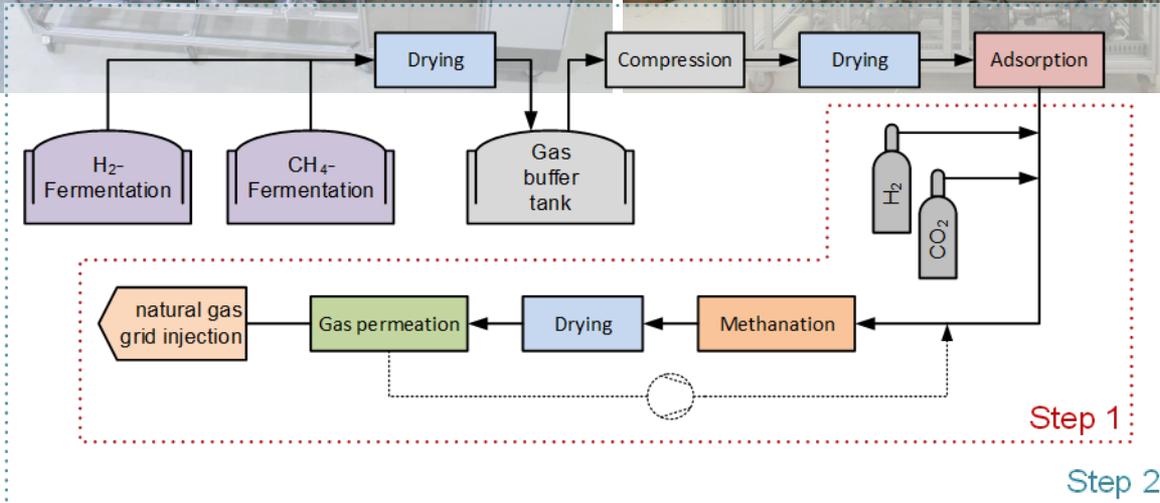
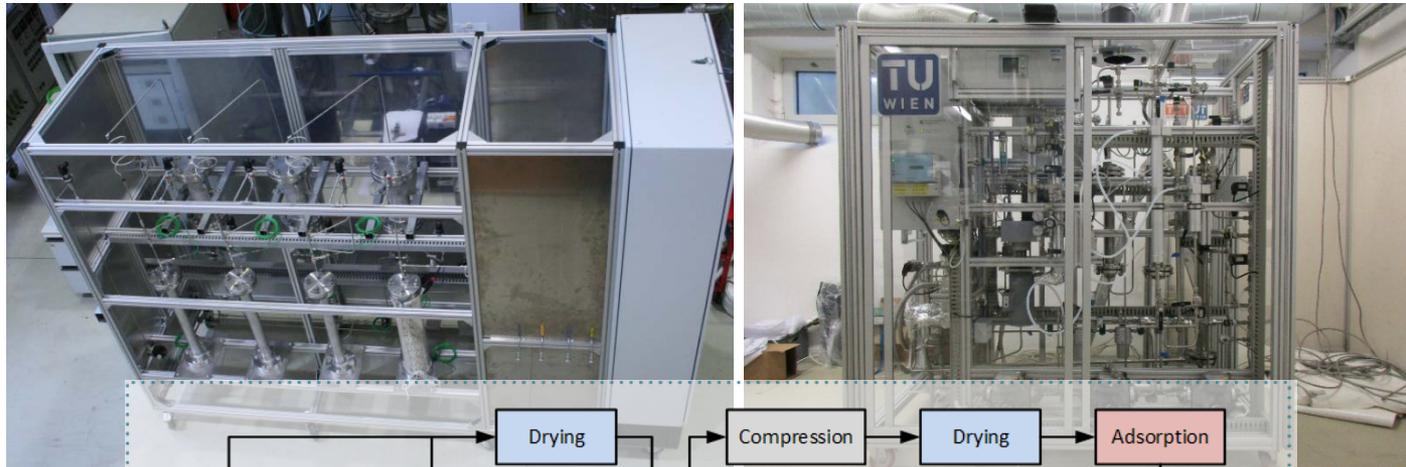
P2G pilot plant experiments – proof of concept

Research Studios Austria – “EE-Methane from CO₂” & “OptFuel”

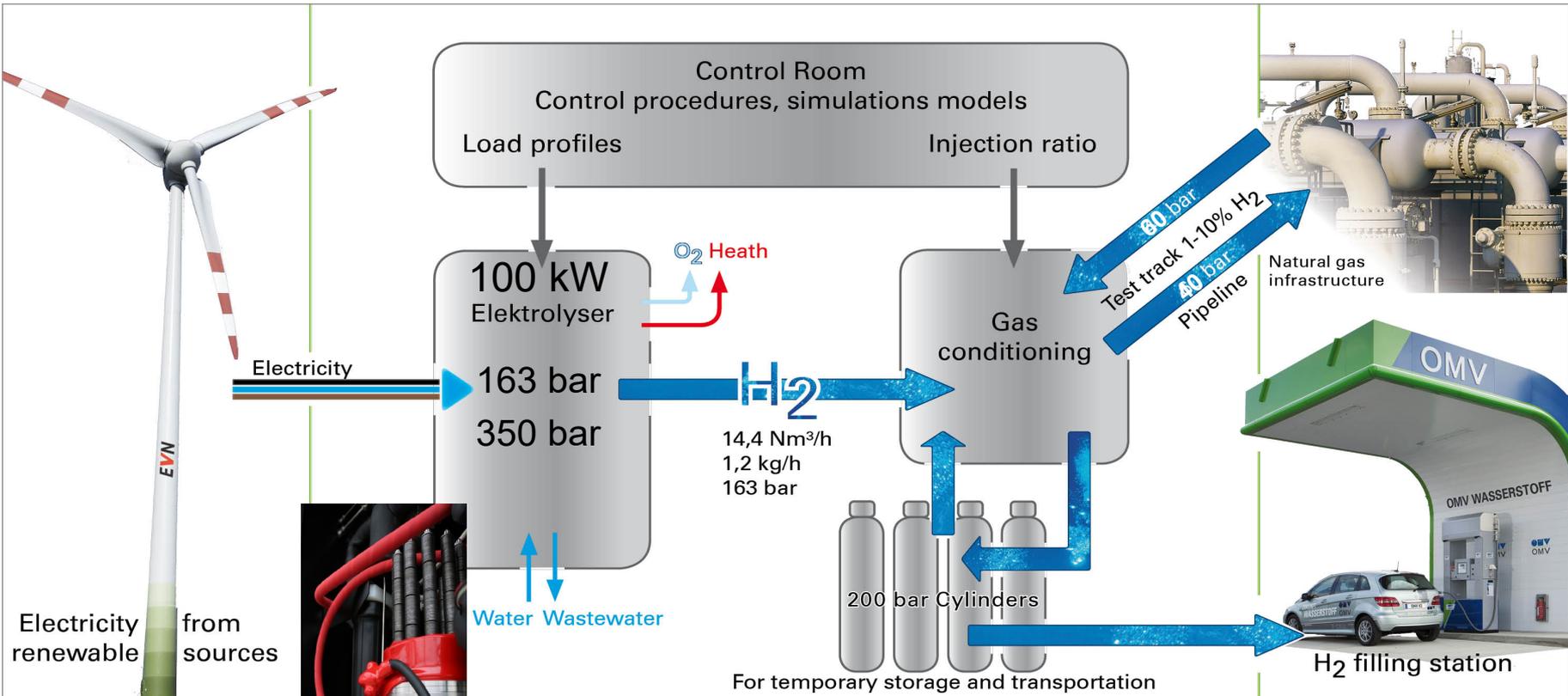
Thermochemical methanation + Gas upgrading for grid injection

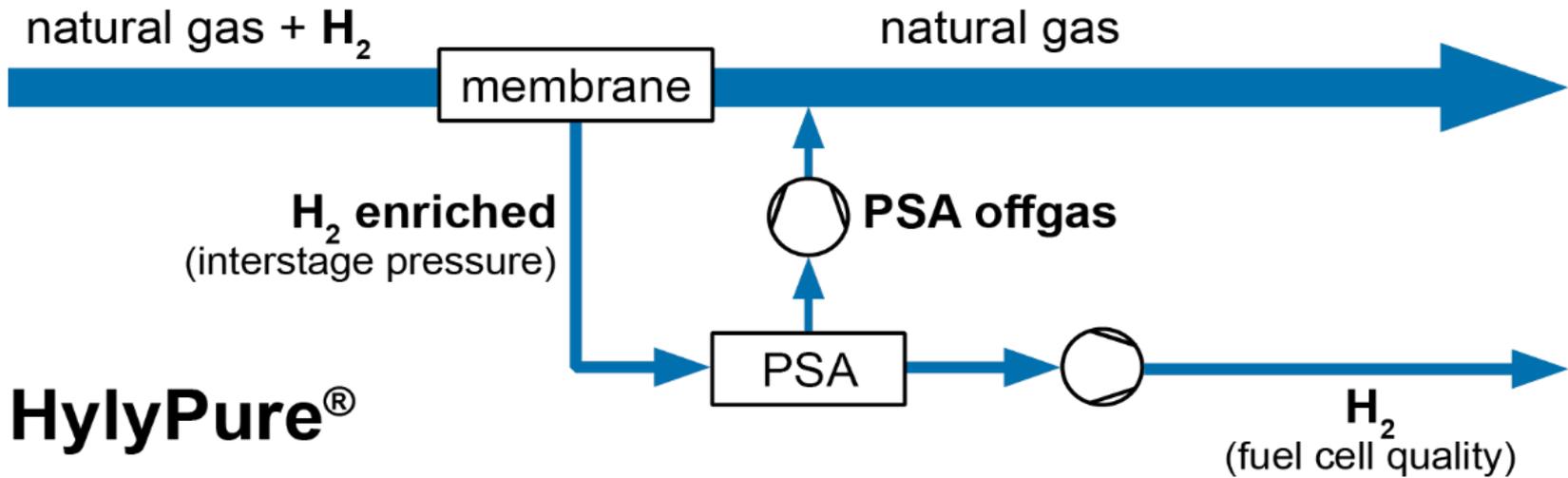
Recycling of unconverted H₂ + CO₂ (membrane permeate)

Key goals: new catalyst, minimize CO in product, maximize conversion, simplify process, pilot tests of process chain, process model for scale-up



Hydrogen for H₂-fuel station and for injection into the natural gas grid – Production of gas mixtures for HylyPure





HylyPure®

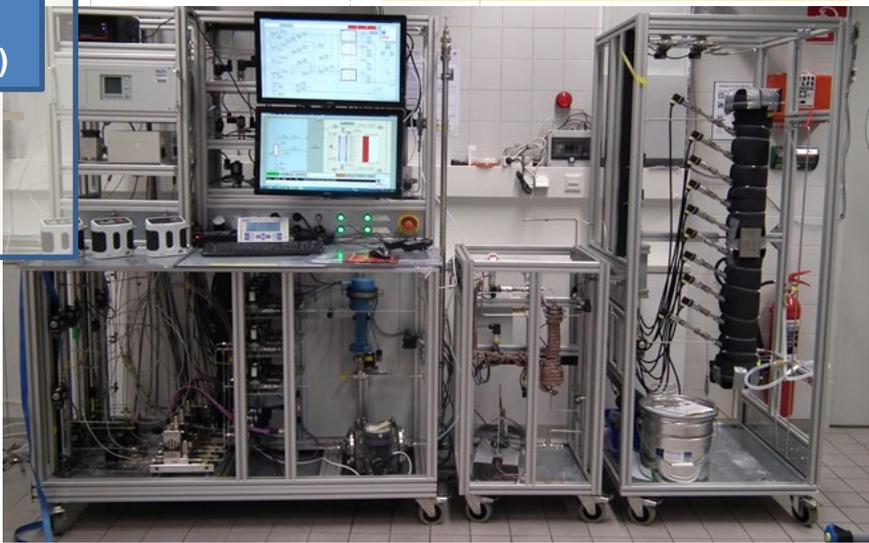
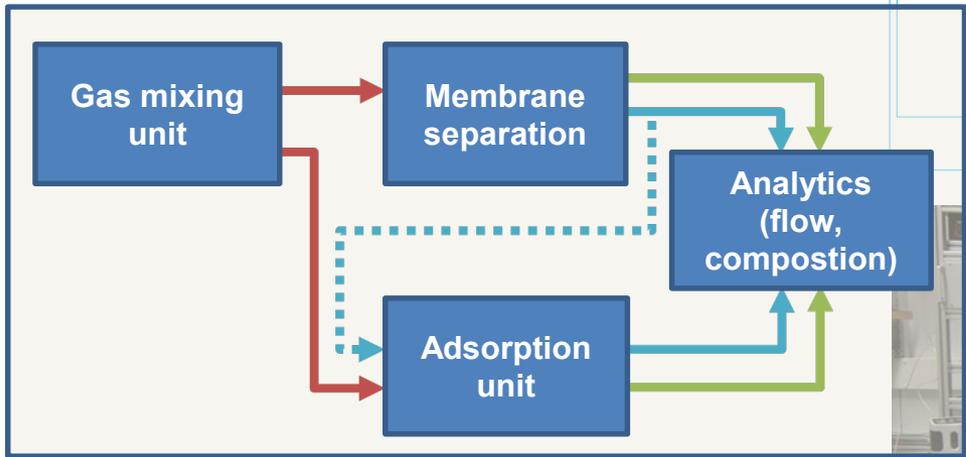
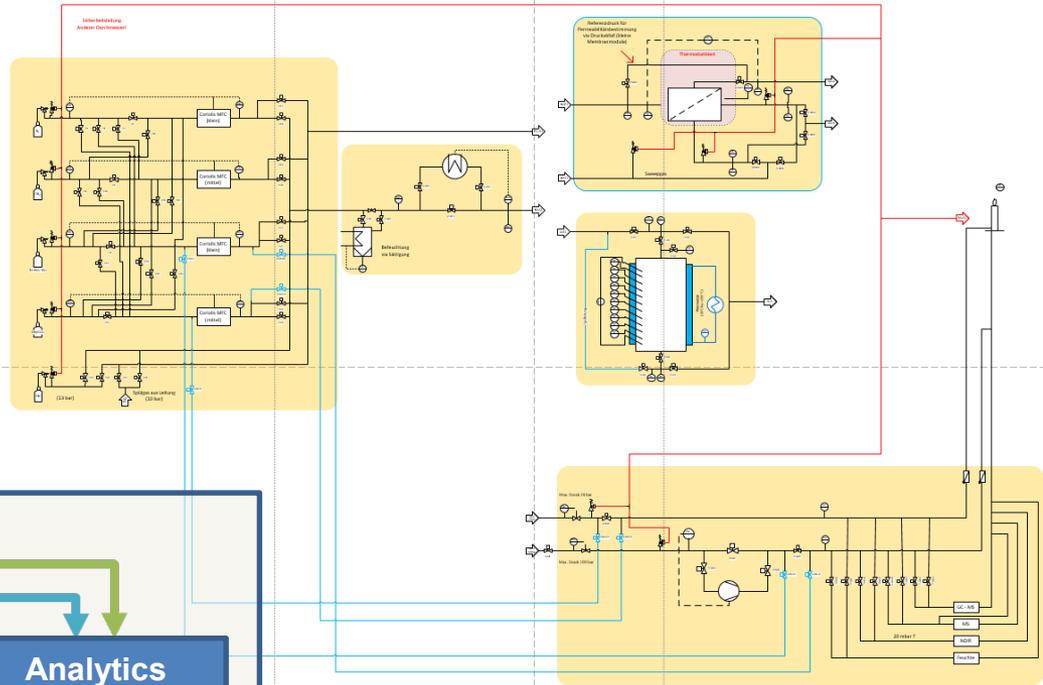
- Combination of several process steps
 - Membrane gas permeation using H₂-selective membranes
 - Pressure swing adsorption (PSA)
 - Final cleaning stage by adsorption

| Feed | Product |
|---|---|
| <ul style="list-style-type: none"> ■ Natural gas <ul style="list-style-type: none"> – CH₄, CO₂, H₂ – C_xH_y, N₂, H₂O, H₂S, etc. ■ Maximum H₂ <ul style="list-style-type: none"> – 4 % (v/v) in Austria – 2%/10 % (v/v) in Germany ■ Pressure levels <ul style="list-style-type: none"> – 70-120 bar (Level 1) – 6-70 bar (Level 2) – < 6 bar (Level 3) | <ul style="list-style-type: none"> ■ Fuel cell quality <ul style="list-style-type: none"> – ISO 14687-2:2012 – min. 99.97 % H₂ – Higher hydrocarbons (as CH₄): 2 ppm – CO₂: 2 ppm ■ Pressure: up to 700 bar |

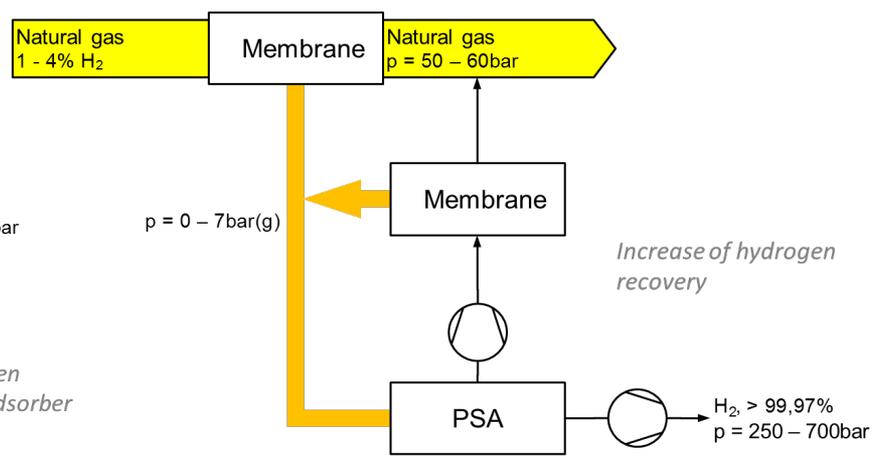
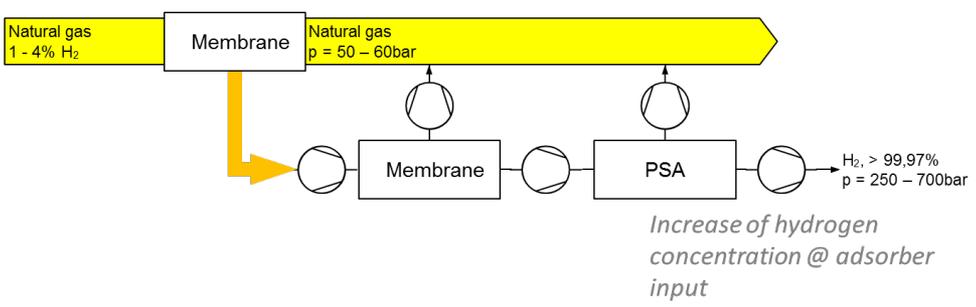
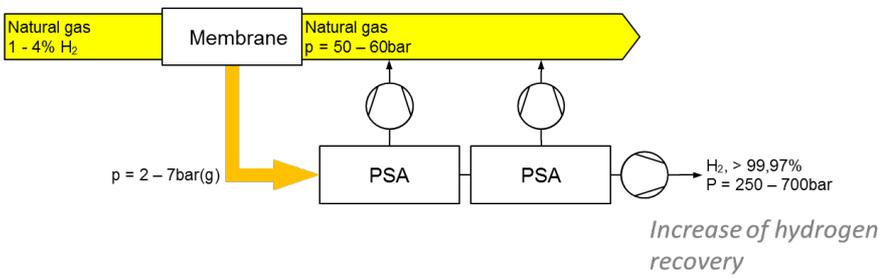
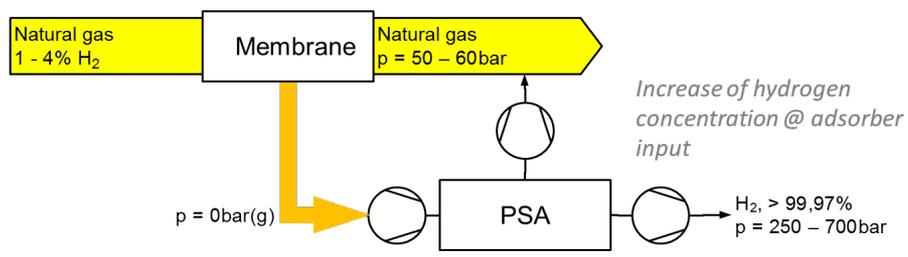
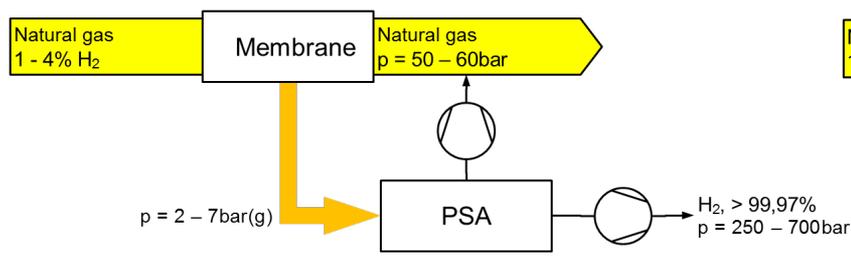


HylyPure® is a project of TU Wien and OMV AG.
HylyPure® is supported by the Austrian Climate and Energy Fund.

- Proof-of-concept @ lab-scale

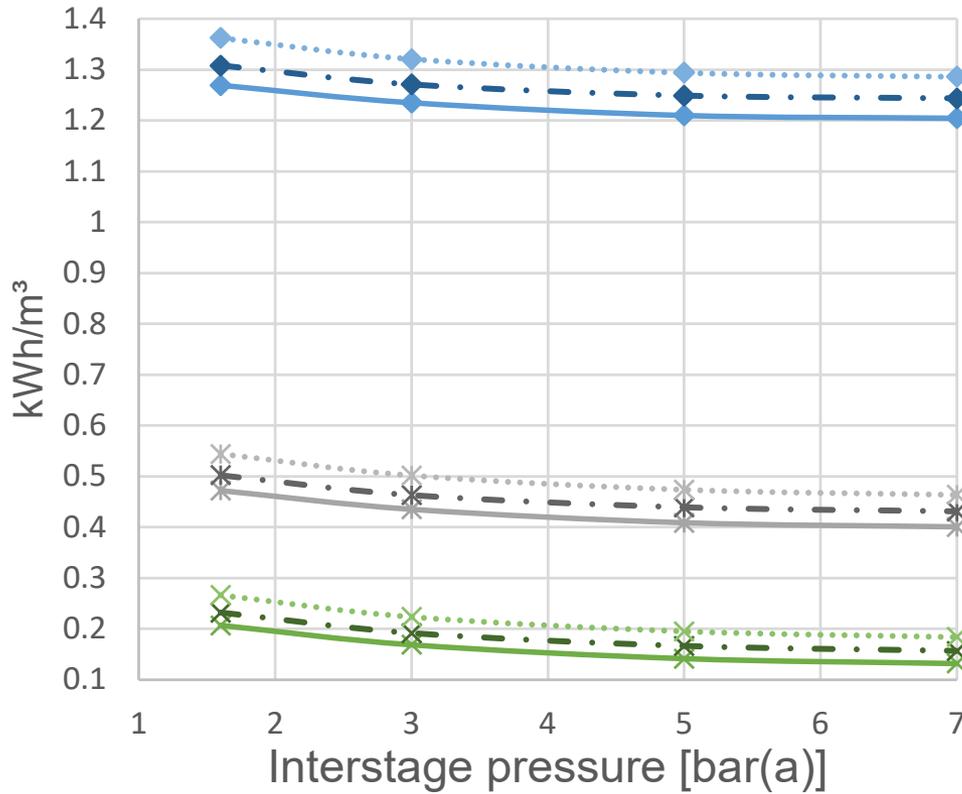


HylyPure® – Process options



Further options possible...

Energy consumption of HylyPure[®] process

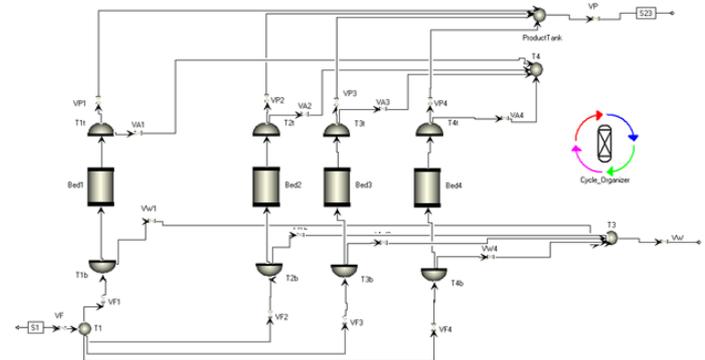


- ◆— Stage-Cut 0.1 Recovery 20 %
- *— Stage-Cut 0.1 Recovery 50 %
- x— Stage-Cut 0.1 Recovery 98 %
- ◆— Stage-Cut 0.15 Recovery 20 %
- *— Stage-Cut 0.15 Recovery 50 %
- x— Stage-Cut 0.15 Recovery 98 %
- ...◆... Stage-Cut 0.2 Recovery 20 %
- ...*... Stage-Cut 0.2 Recovery 50 %
- ...x... Stage-Cut 0.2 Recovery 98 %

Reference process: Decentral hydrogen production by water electrolysis

Energy consumption: 4.2-4.8 kWh/m³; Delivery pressure: 25.81 bar(a)

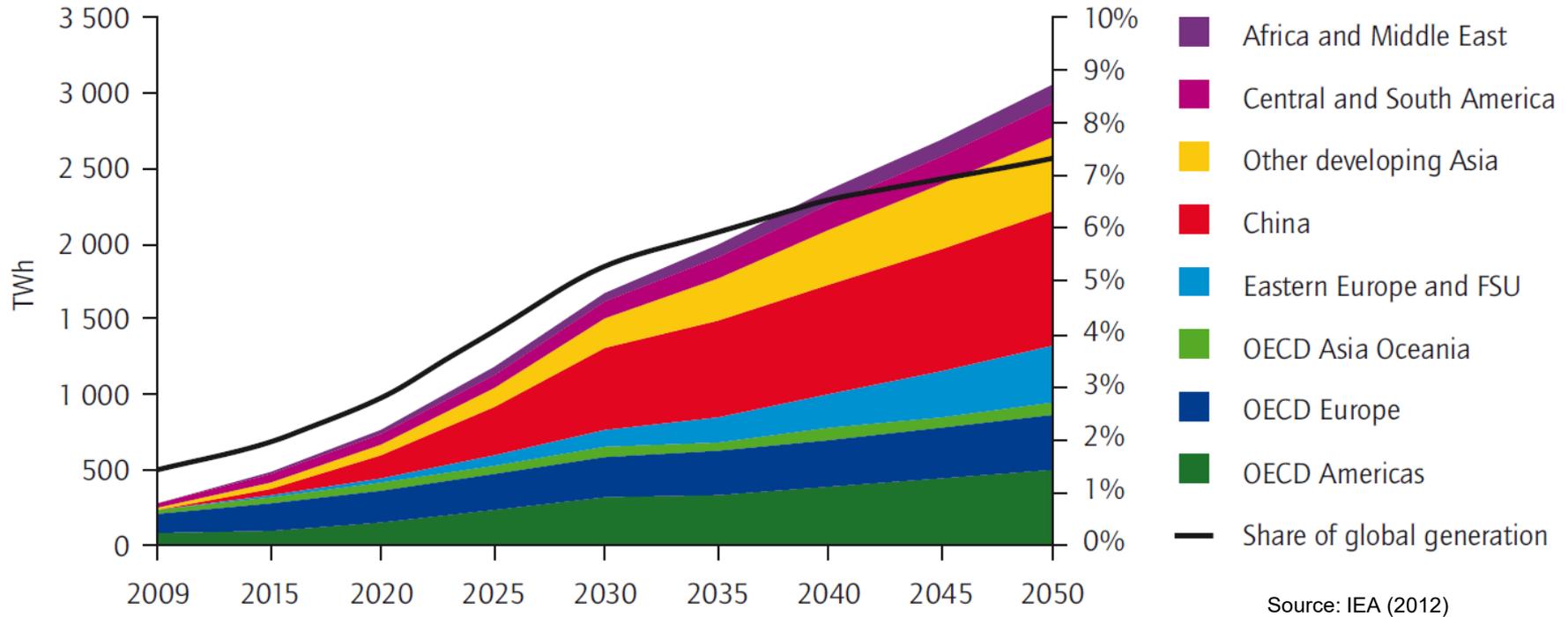
(Ivy, 2014 – Summary of electrolytic hydrogen production. Milestone completion report, Golden, Colorado)



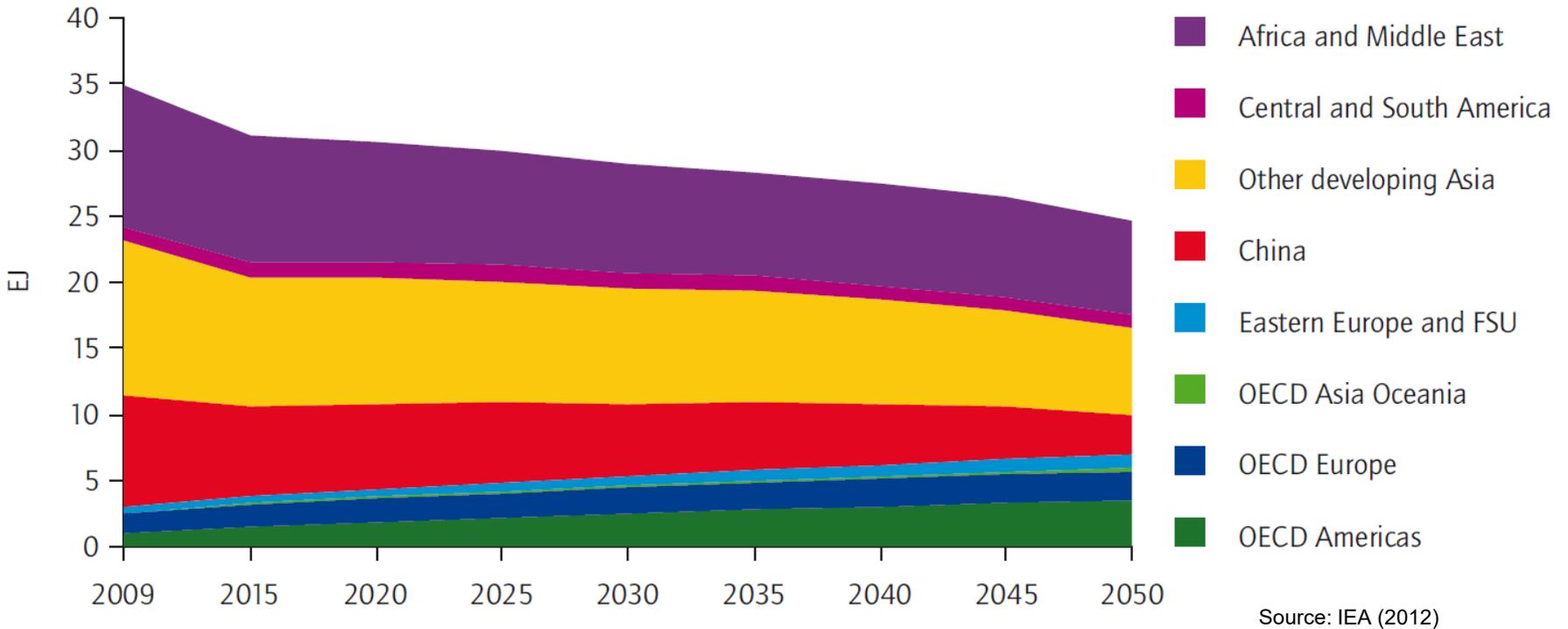
Rightsizing ...





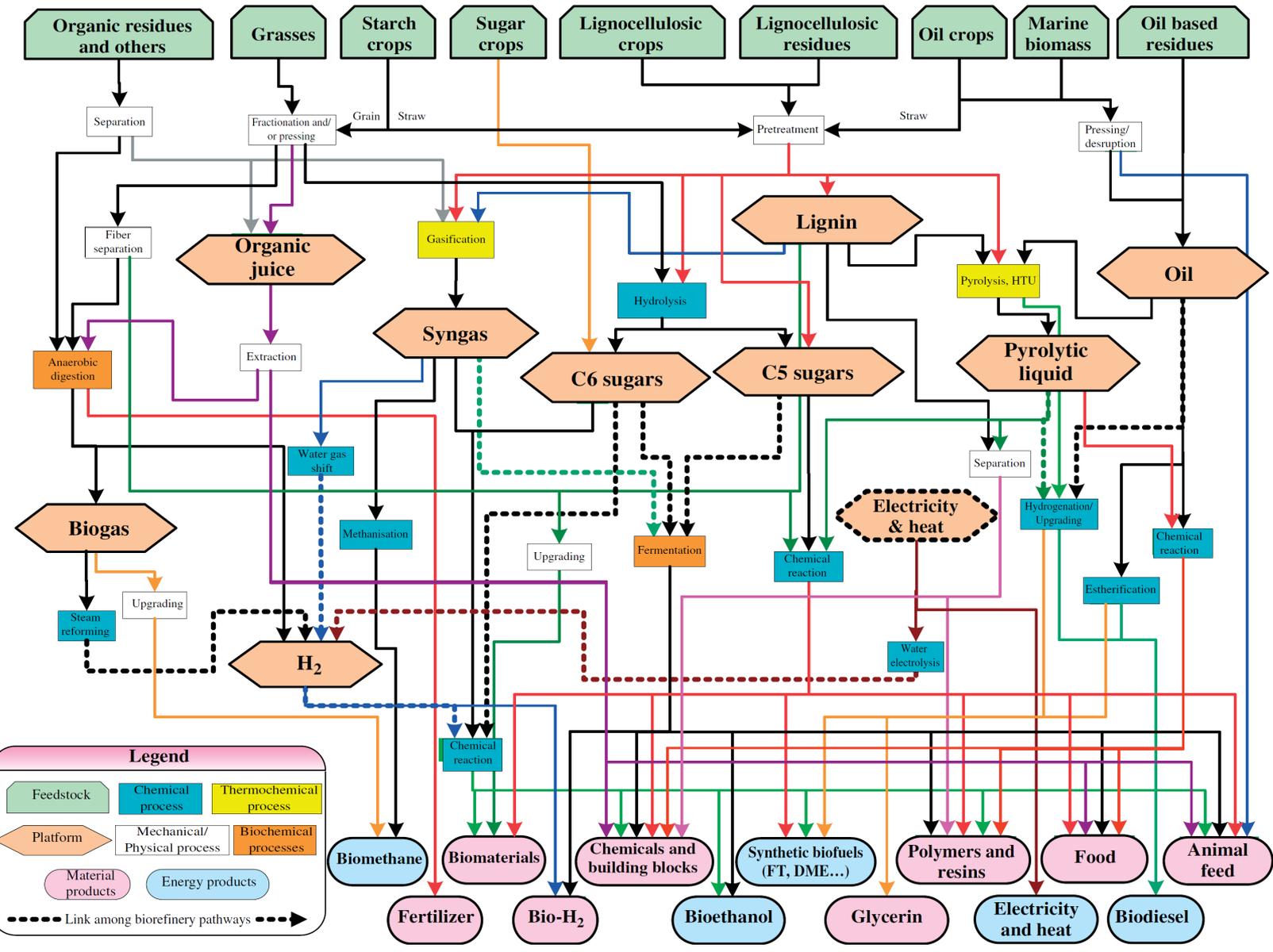


In 2050, IEA estimates 2 460 TWh of electricity will be produced from biomass and waste, a fivefold increase on 2010



Final bioenergy consumption in the buildings sector in different world regions

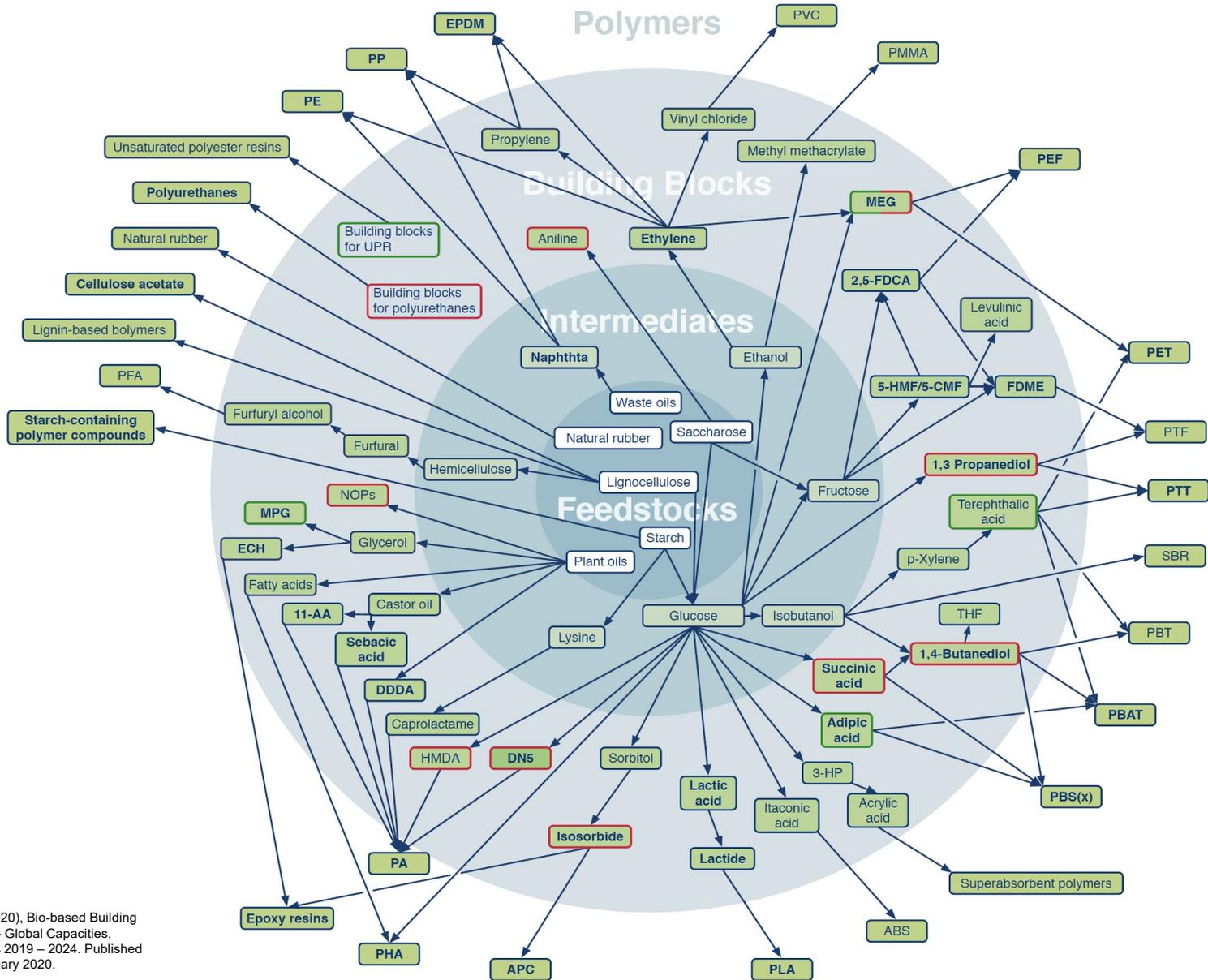
And the Future?



Biorefinery systems network – IEA Task 42

Biorefineries: bio-based building blocks and polymers

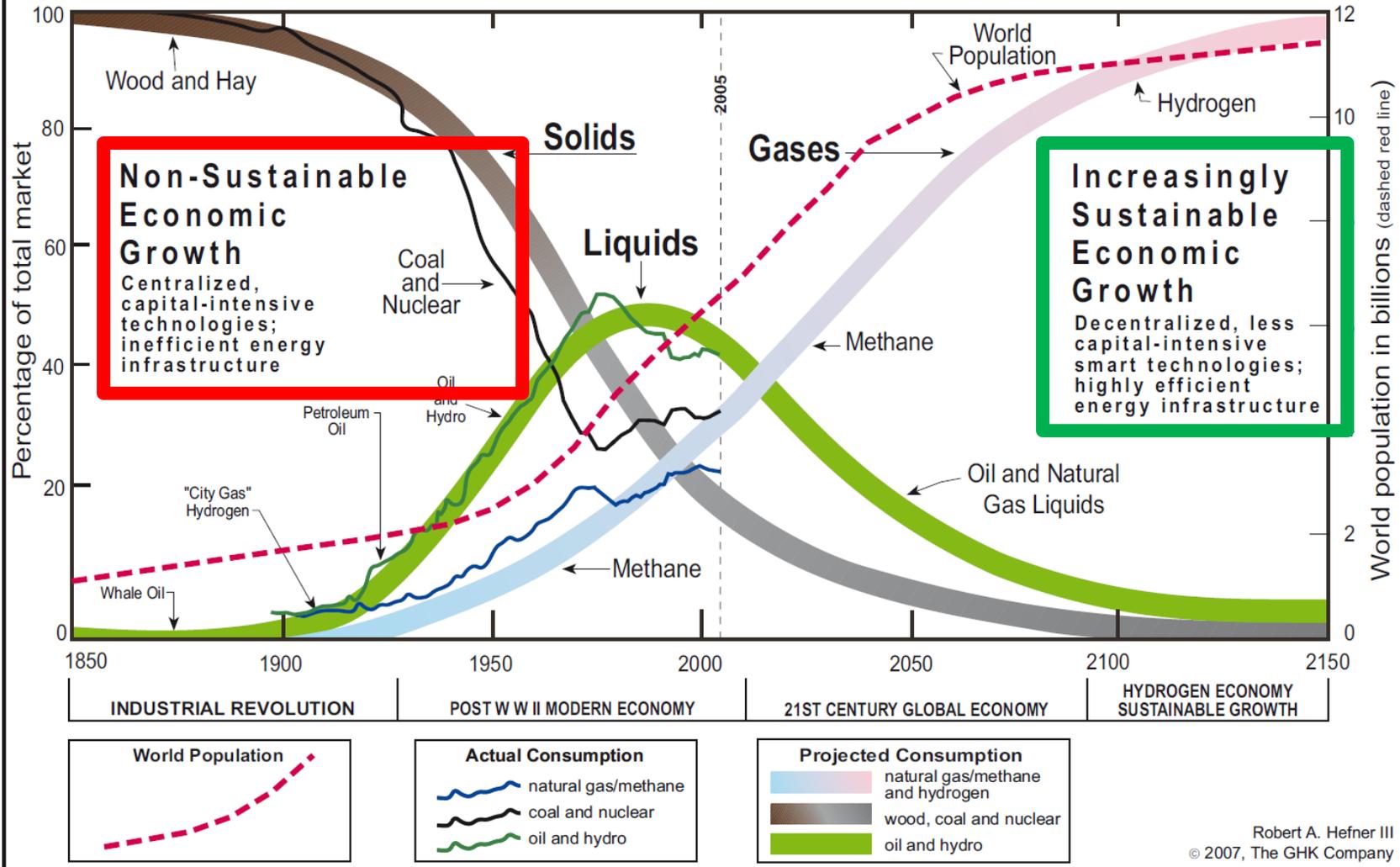
Biorefineries and beyond...



Koczinski, P., et al. (2020). Bio-based Building Blocks and Polymers – Global Capacities, Production and Trends 2019 – 2024. Published by Nova Institute, January 2020.

The Age of Energy Gases?

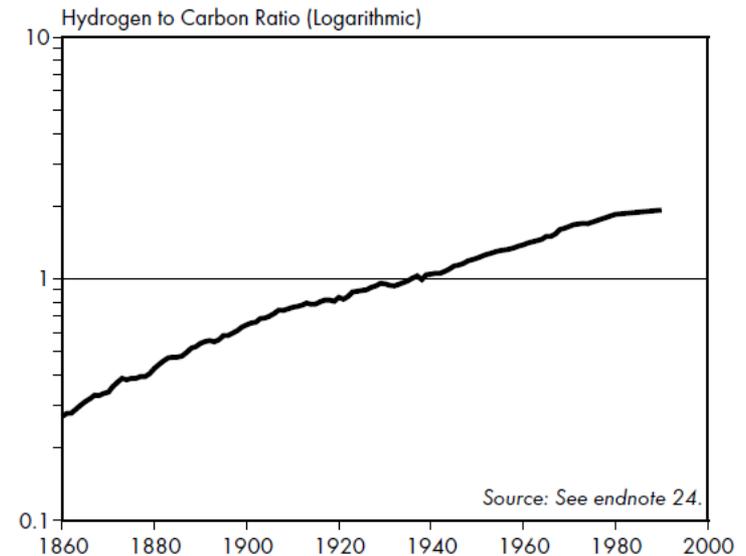
The Age of Energy Gases Global Energy Transition Waves



Robert A. Hefner III
© 2007, The GHK Company

- Biomass to grid is more than power!
- Polygeneration technology options available
- Thermochemical and biochemical routes dependent on biomass composition
- These routes will also contribute to the production of sustainable biofuels
- Electricity from biomass share on global energy production to rise in the next decades

Hydrogen-Carbon Ratio, World Energy Mix, 1860–1990



Thank you for your attention!



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